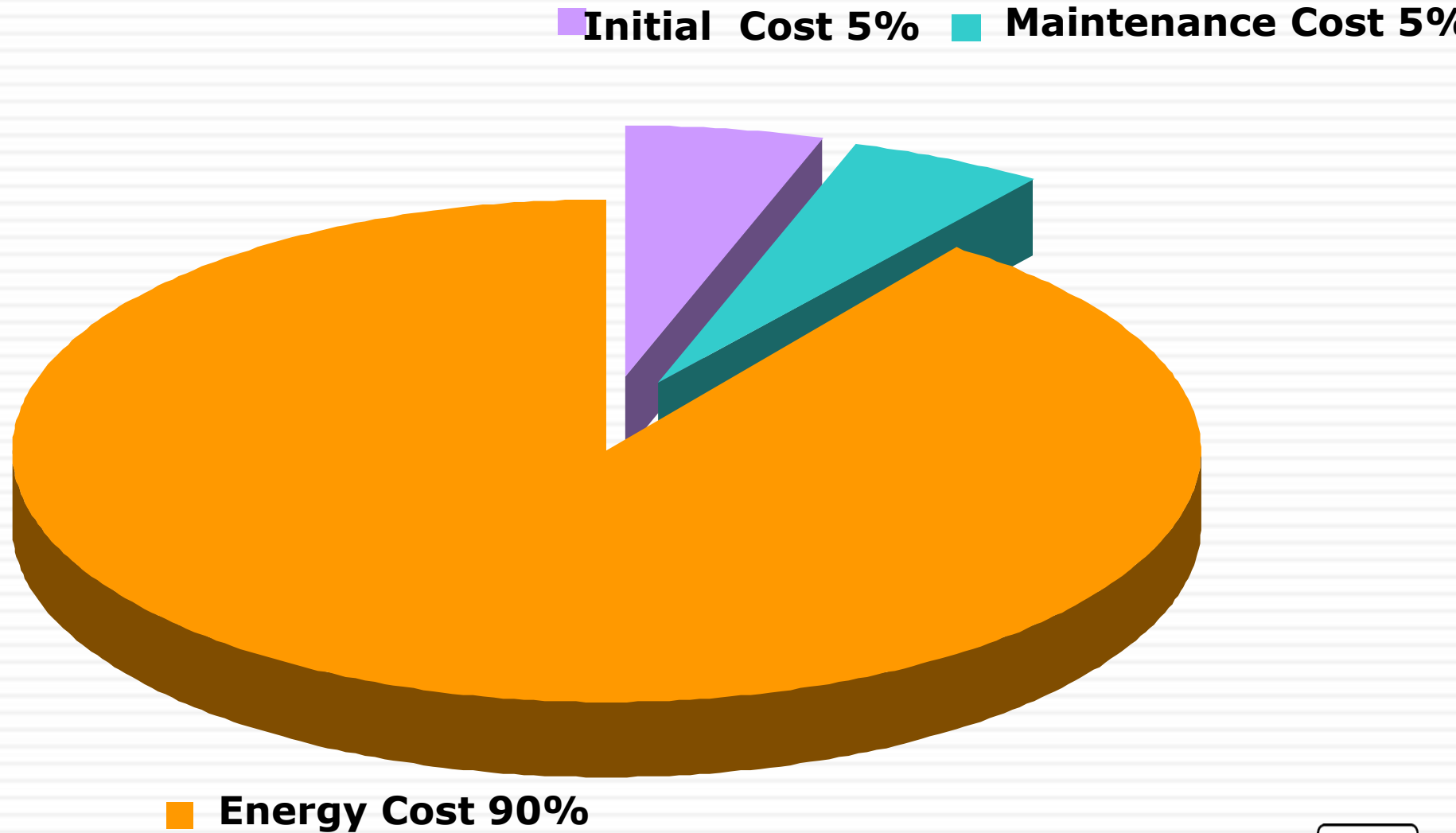


# UTILITY SYSTEM – COMPRESSORS AND PUMPS

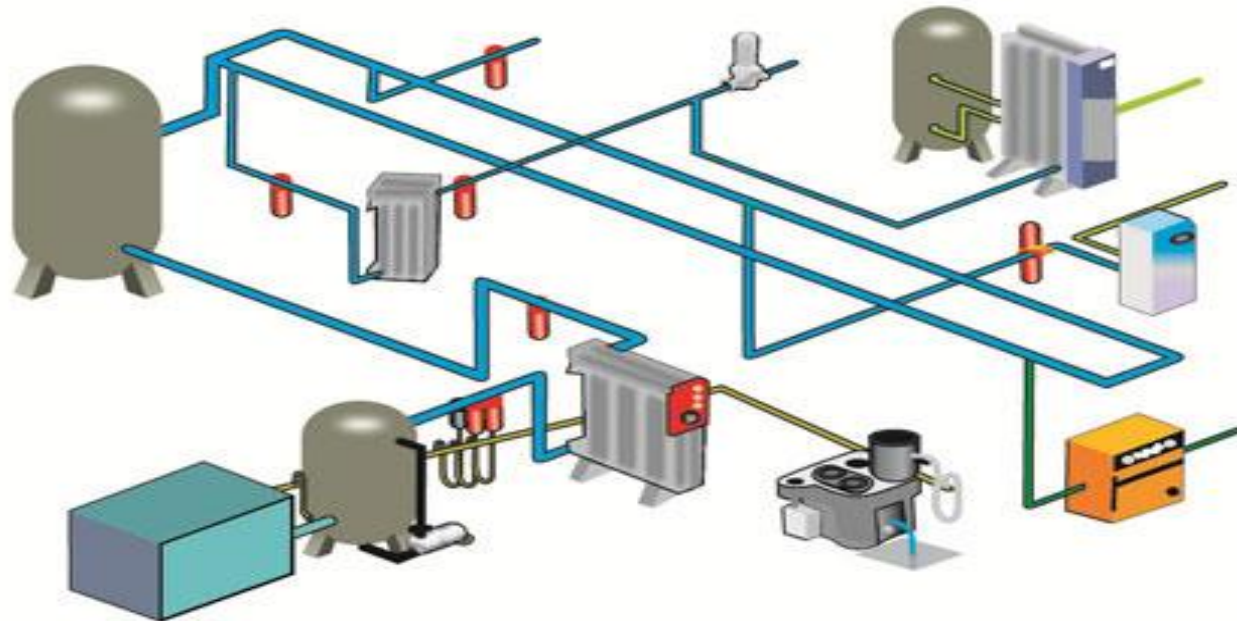


Confederation of Indian Industry

# Life Cycle Cost

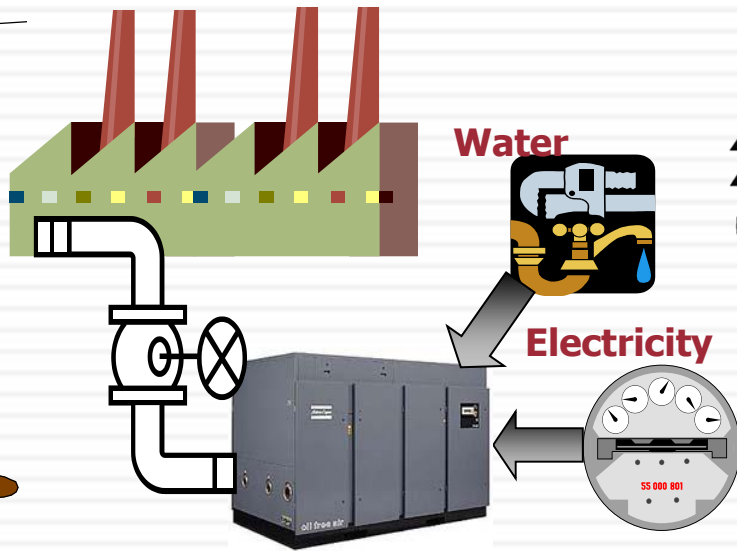
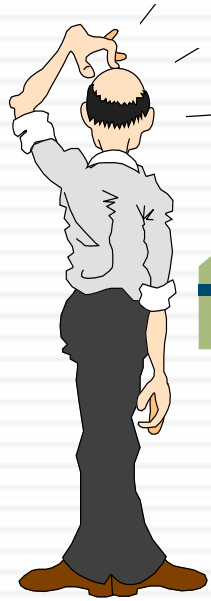


# COMPRESSED AIR SYSTEM



# Energy Cost of Running Air Compressor

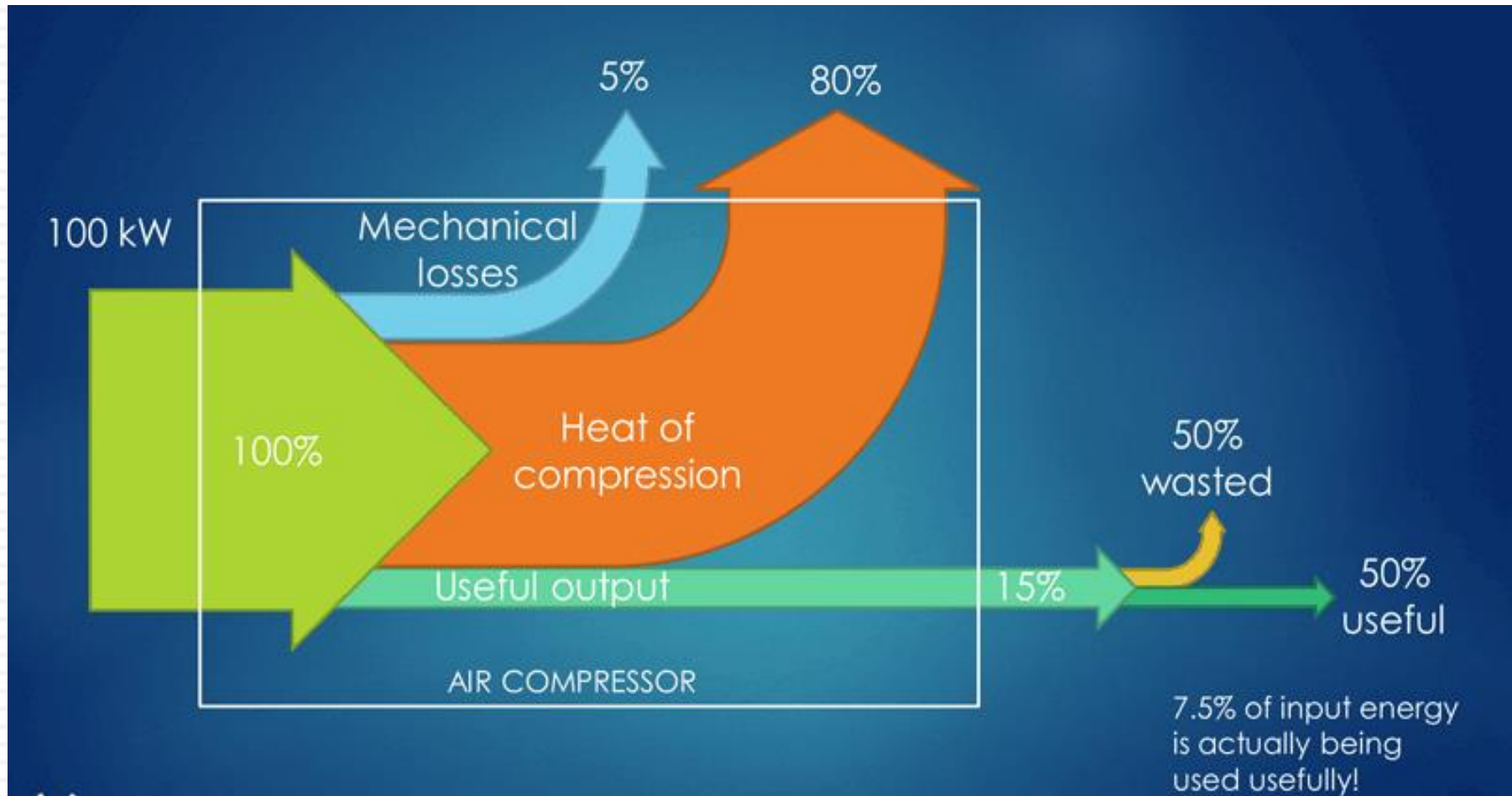
**90 kW Compressor running continuously consumes  $\approx$  600,000 kWh annually**



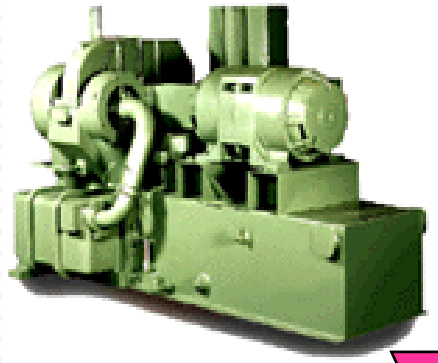
**@ rate of Rs. 6/kWh,  
Costs Rs. 36 Lacs/year**

***Which is 4 times the cost of  
Compressor itself !!***

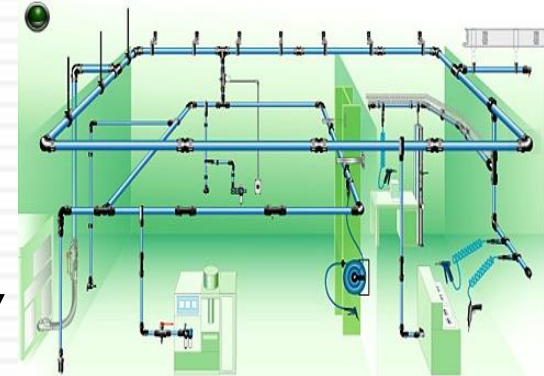
# Sankey Diagram of Compressed Air System



# Compressed Air: Most Expensive Form of Energy!



Compressor  $\eta$  & Installation



Compressed Air System  
Installation  
Comp Acc + Piping + Design

**EFFICIENCY**

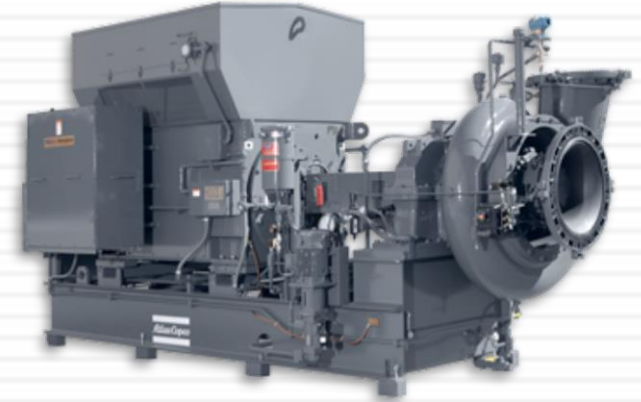
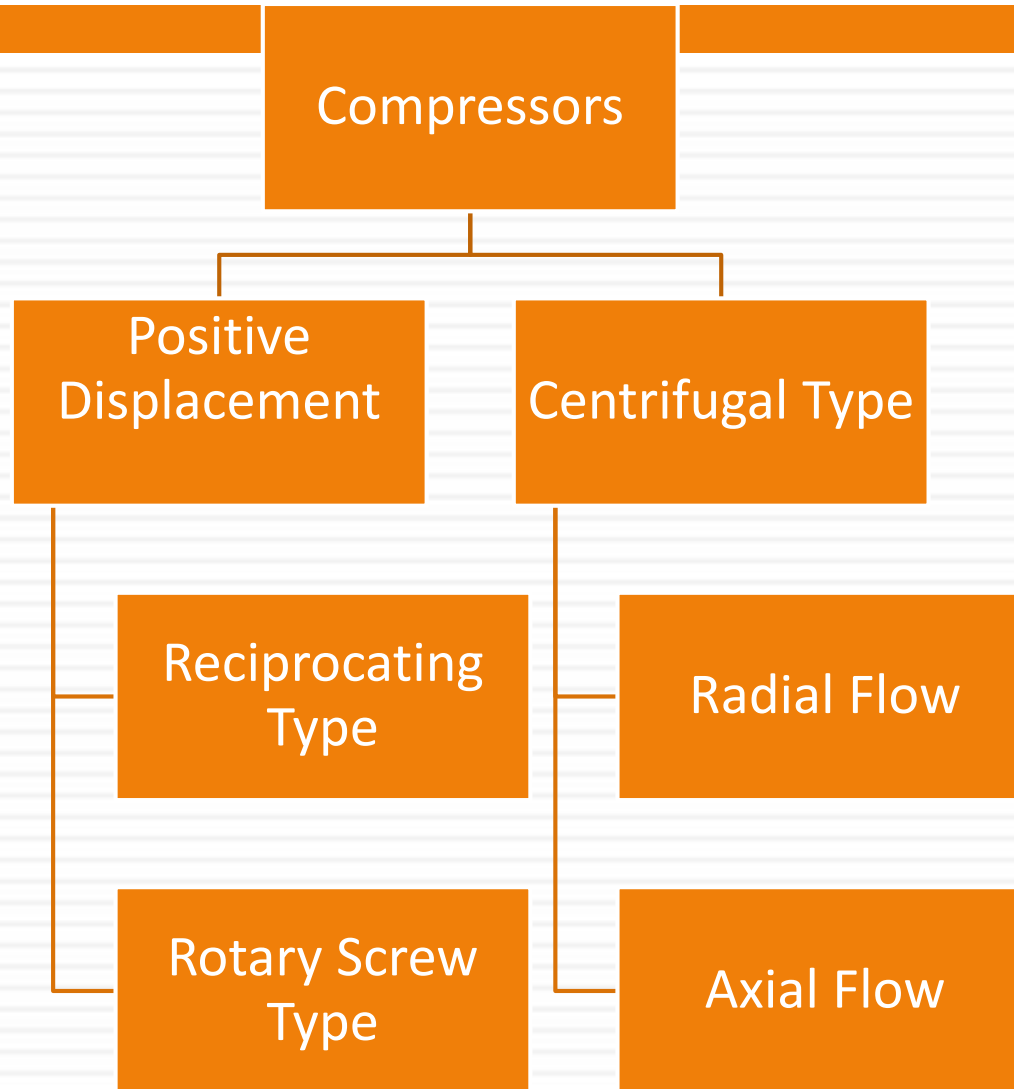
Sustenance



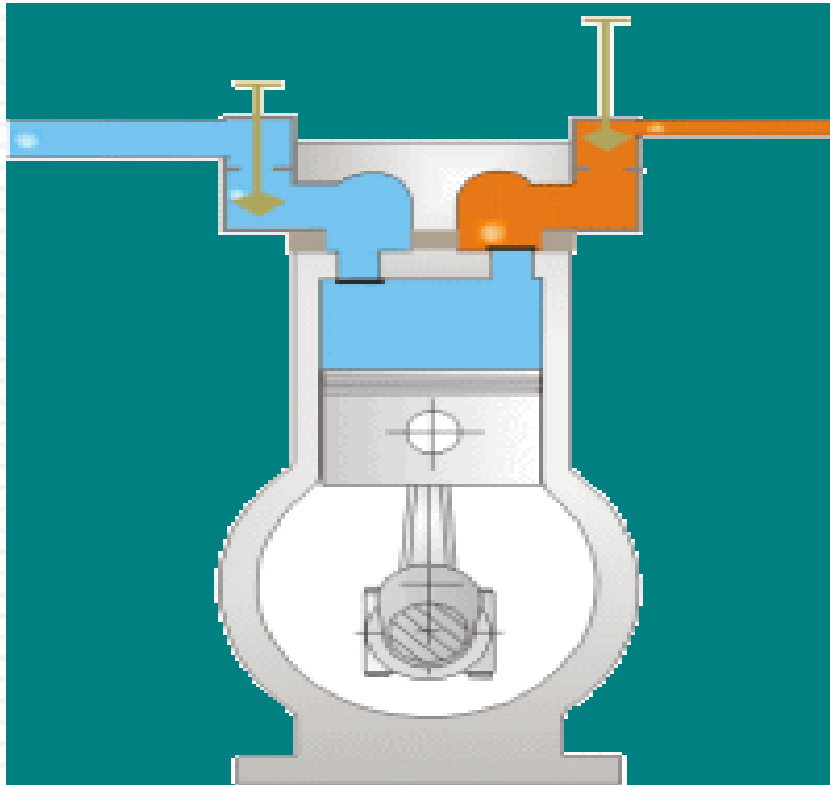
Efficiency in Air Utilisation



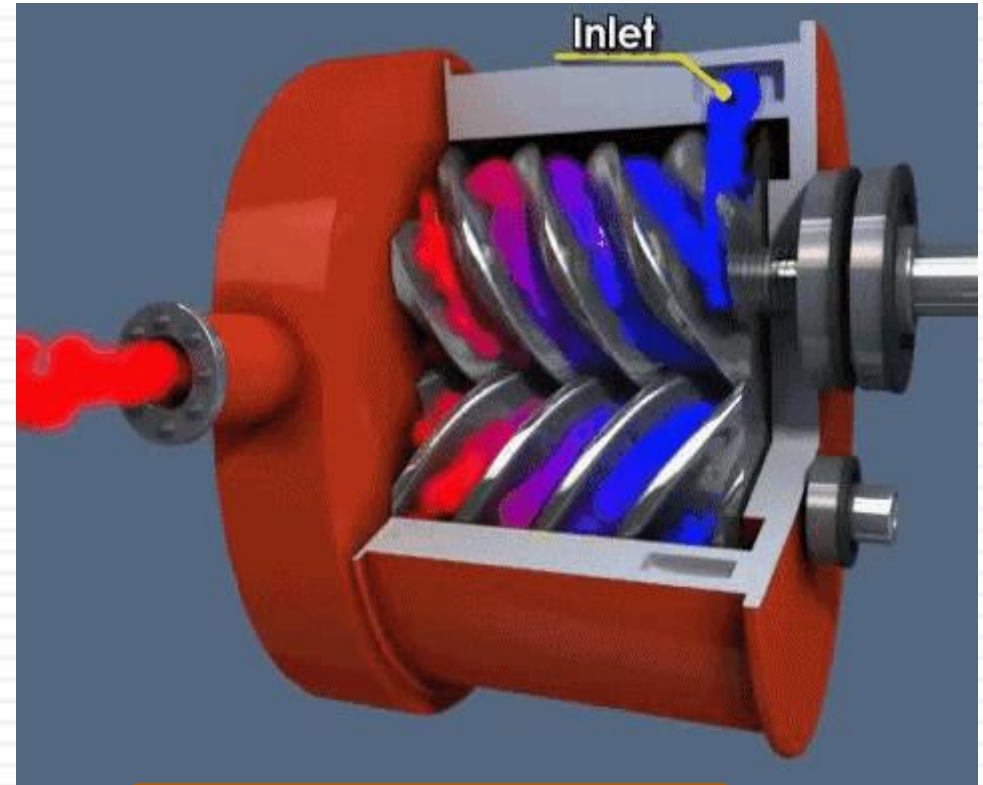
# Air Compressors



# Reciprocating and Screw Compressor



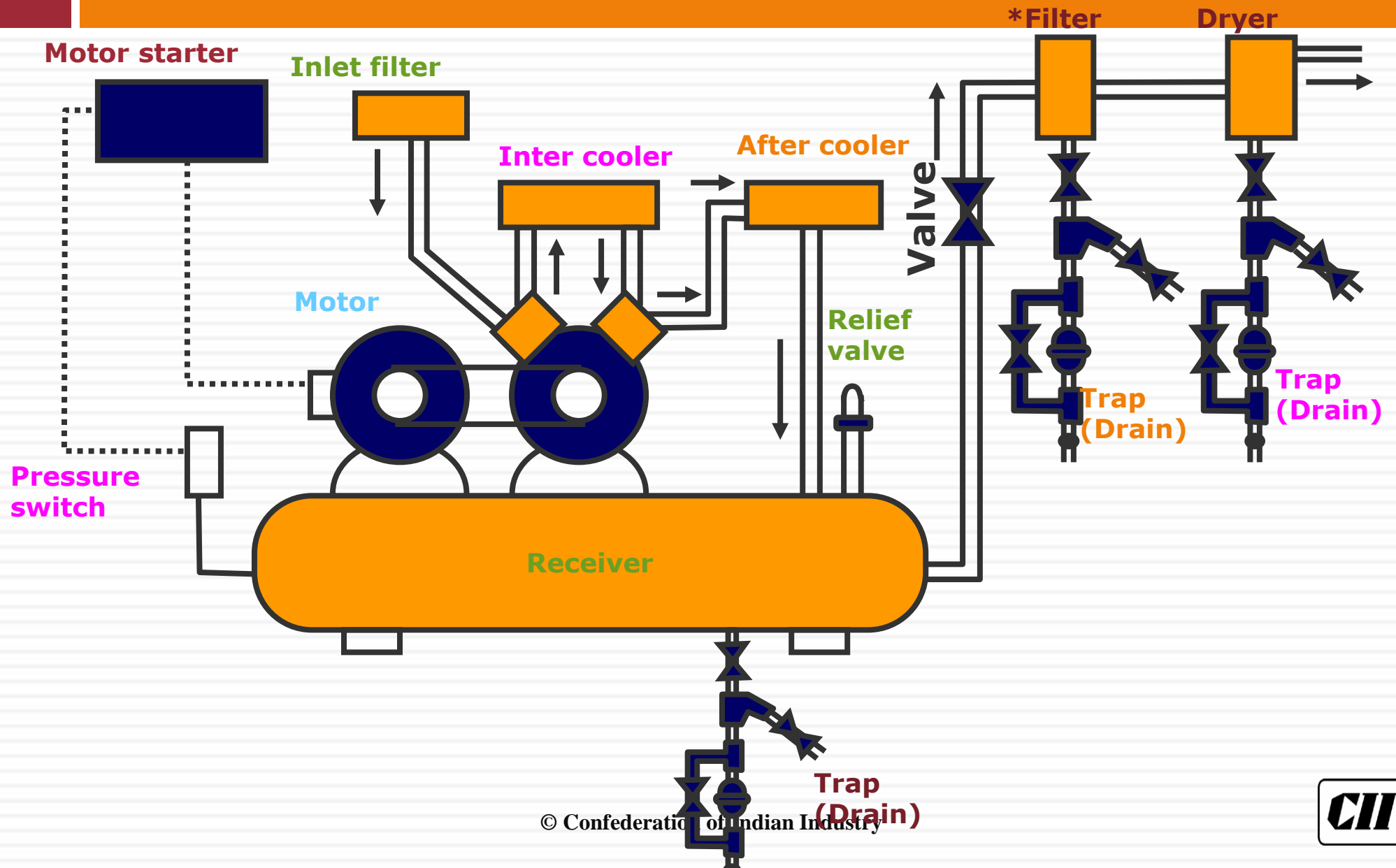
Reciprocating Compressor



Rotary Screw Compressor



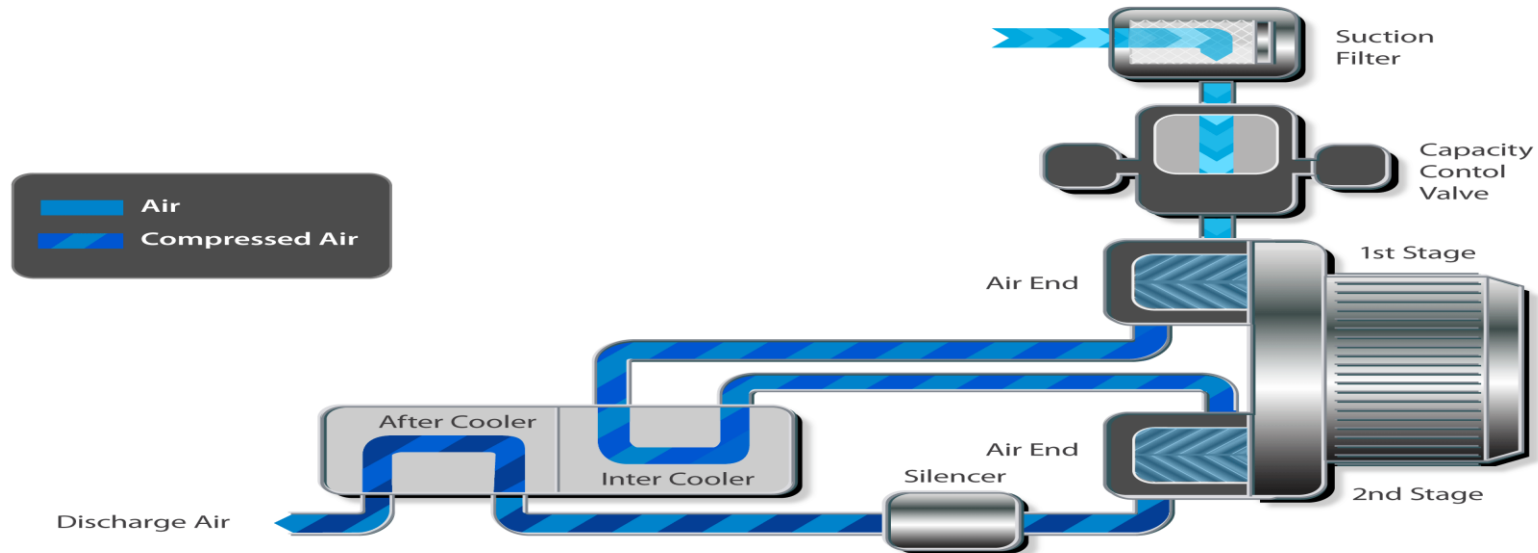
# Two Stage Reciprocating Compressor



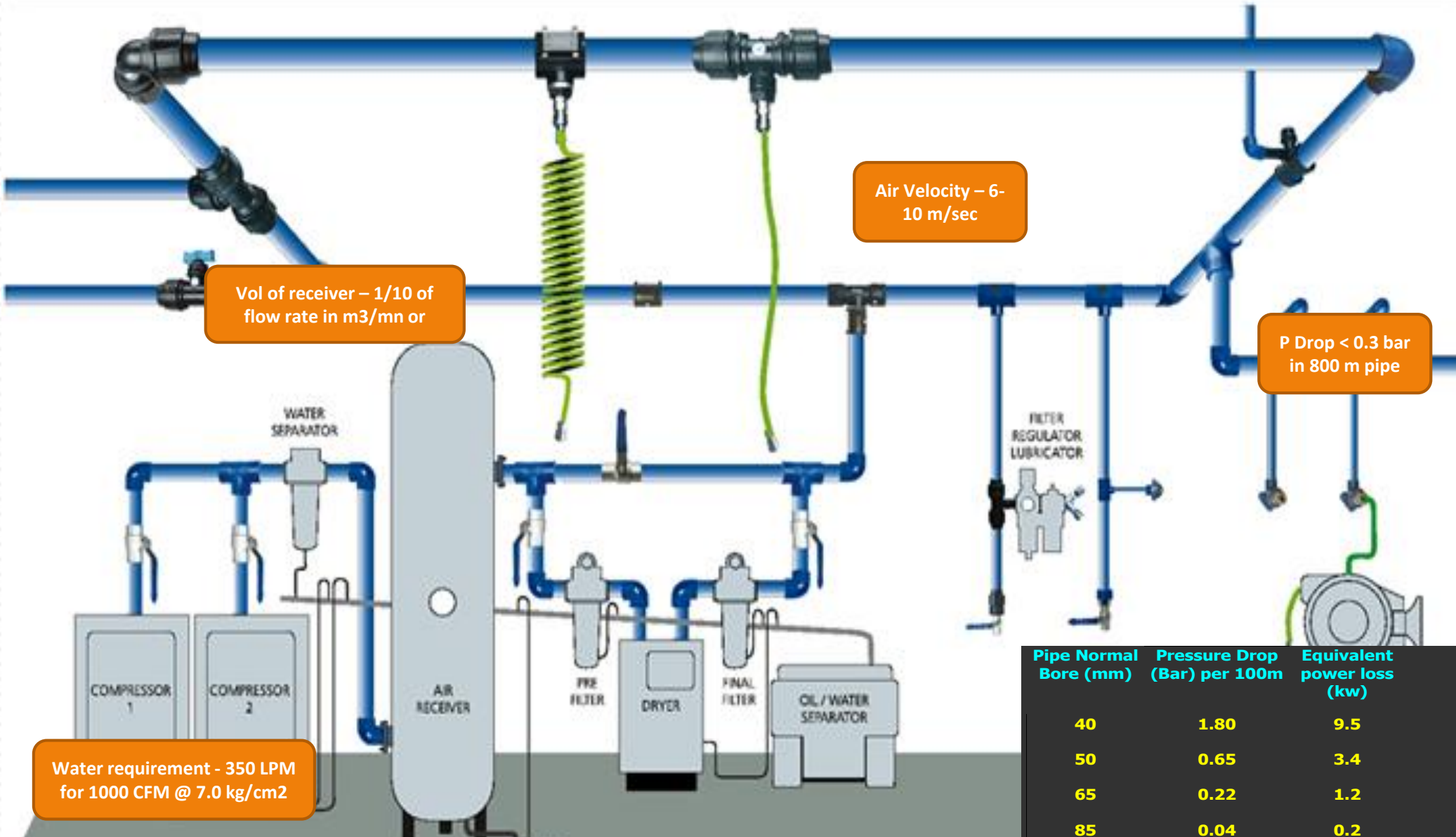
# Inter-cooler & After cooler

- Inter cooling reduces temperature & volume
- After cooler reduces the moisture

## Inter cooler and After cooler



# Recommended Installation



Vol of receiver – 1/10 of flow rate in m<sup>3</sup>/mn or

Air Velocity – 6-10 m/sec

P Drop < 0.3 bar in 800 m pipe

Water requirement - 350 LPM for 1000 CFM @ 7.0 kg/cm<sup>2</sup>

Pipe Normal Bore (mm)	Pressure Drop (Bar) per 100m	Equivalent power loss (kw)
40	1.80	9.5
50	0.65	3.4
65	0.22	1.2
85	0.04	0.2

# Capacity Test (Pumping Method)

$$\text{Average Compressor Delivery} = \frac{P_2 - P_1}{P} \cdot V_R \cdot \frac{1}{\Delta t}$$

$P_1$  = Initial pressure in receiver

$P_2$  = Final pressure in receiver

$P$  = Atmospheric pressure

$V_R$  = Volume of air receiver

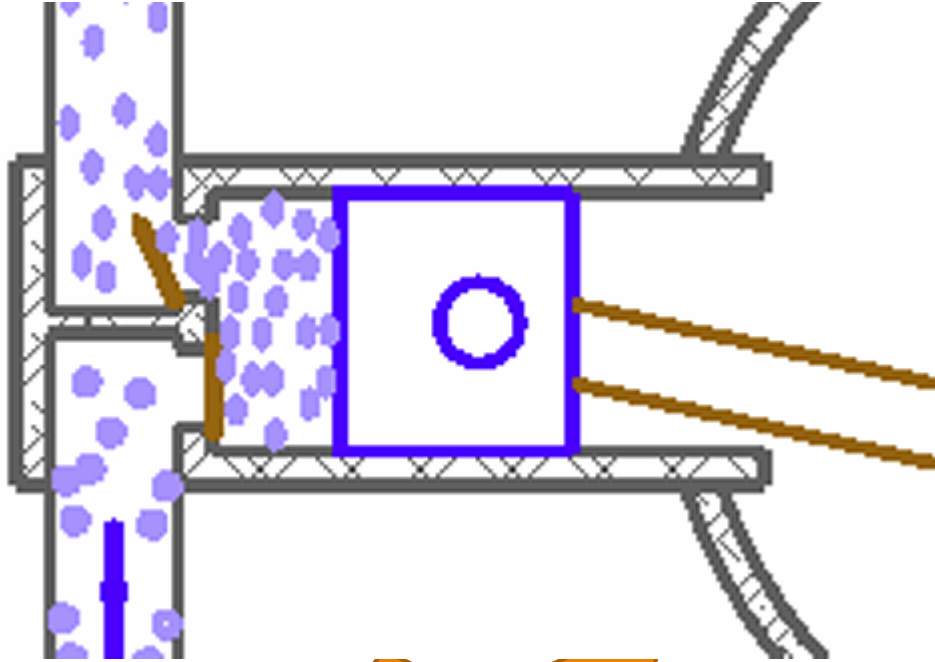
$\Delta t$  = Time taken for charging the receiver from  $P_1$  to  $P_2$



# Check list for efficient operation of Compressor



# Dry Air Intake

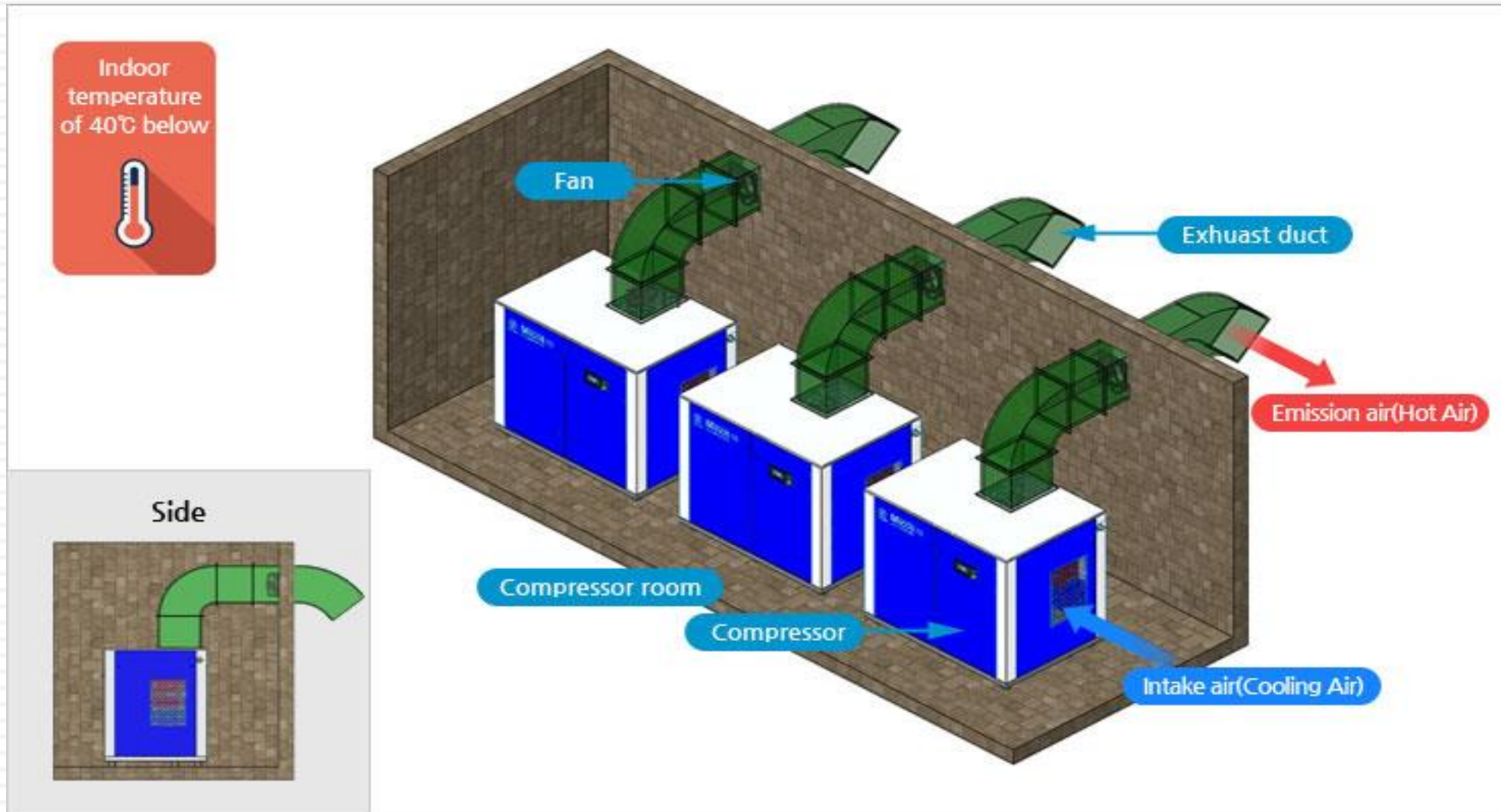


**TABLE 3.2 EFFECT OF INTAKE AIR TEMPERATURE ON POWER CONSUMPTION**

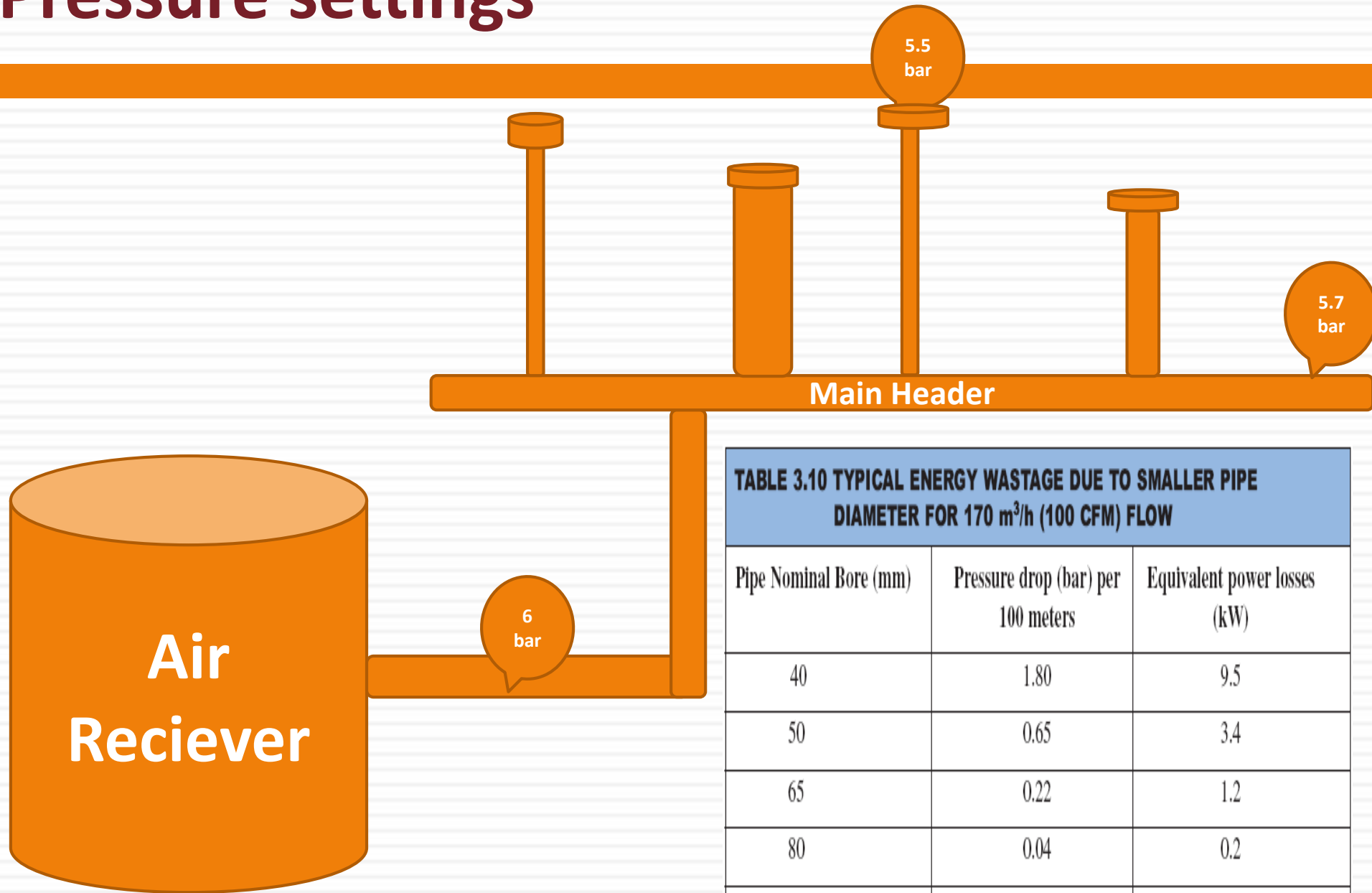
Inlet Temperature (°C)	Relative Air Delivery (%)	Power Saved (%)
10.0	102.0	+ 1.4
15.5	100.0	Nil
21.1	98.1	- 1.3
26.6	96.3	- 2.5
32.2	94.1	- 4.0
37.7	92.8	- 5.0
43.3	91.2	- 5.8

Every 4°C rise in inlet air temperature results in a higher energy consumption by 1 % to achieve equivalent output

# Compressor Room



# Pressure settings



**TABLE 3.10 TYPICAL ENERGY WASTAGE DUE TO SMALLER PIPE DIAMETER FOR 170 m<sup>3</sup>/h (100 CFM) FLOW**

Pipe Nominal Bore (mm)	Pressure drop (bar) per 100 meters	Equivalent power losses (kW)
40	1.80	9.5
50	0.65	3.4
65	0.22	1.2
80	0.04	0.2
100	0.02	0.1



# Operation of compressors

- **5 compressors available**
  - ▣ **660 CFM, 7.5 bar, 110 kW**
- **3 compressors are required to be operated**

# Operation of Compressors

No
CP1
CP2
CP3
CP4
CP5

# Operation of Compressors

No	kW
<b>CP1</b>	<b>110</b>
<b>CP2</b>	<b>90</b>
<b>CP3</b>	<b>100</b>
<b>CP4</b>	<b>105</b>
<b>CP5</b>	<b>95</b>

# Operation of Compressors

No	kW	FAD
<b>CP1</b>	<b>110</b>	<b>660</b>
<b>CP2</b>	<b>90</b>	<b>500</b>
<b>CP3</b>	<b>100</b>	<b>600</b>
<b>CP4</b>	<b>105</b>	<b>645</b>
<b>CP5</b>	<b>95</b>	<b>470</b>

# Operation of Compressors

No	kW	FAD	kW / CFM
<b>CP1</b>	<b>110</b>	<b>660</b>	<b>0.17</b>
<b>CP2</b>	<b>90</b>	<b>500</b>	<b>0.18</b>
<b>CP3</b>	<b>100</b>	<b>600</b>	<b>0.17</b>
<b>CP4</b>	<b>105</b>	<b>645</b>	<b>0.16</b>
<b>CP5</b>	<b>95</b>	<b>470</b>	<b>0.20</b>

***Always select compressor  
based on SEC (kW/CFM) not on  
kW and CFM separately***

# Comparison of Specific Power Consumption

	<b>Reciprocating</b>	<b>Centrifugal</b>	<b>Screw (Single stage)</b>	<b>Screw (Multi stage)</b>
<b>FAD</b>	<b>3950 CFM at 7kg/cm<sup>2</sup></b>			
<b>kW</b>	<b>549</b>	<b>515</b>	<b>632</b>	<b>510</b>
<b>Specific Power (kW/CFM)</b>	<b>0.139</b>	<b>0.130</b>	<b>0.162</b>	<b>0.129</b>

# Replacement of Inefficient Compressor

SEC – 0.21 kW/CFM  
Power Consumption – 21 kW



New Screw Compressor  
SEC – 0.16 kW/CFM  
Power Consumption – 16 kW



Power Savings 25 %

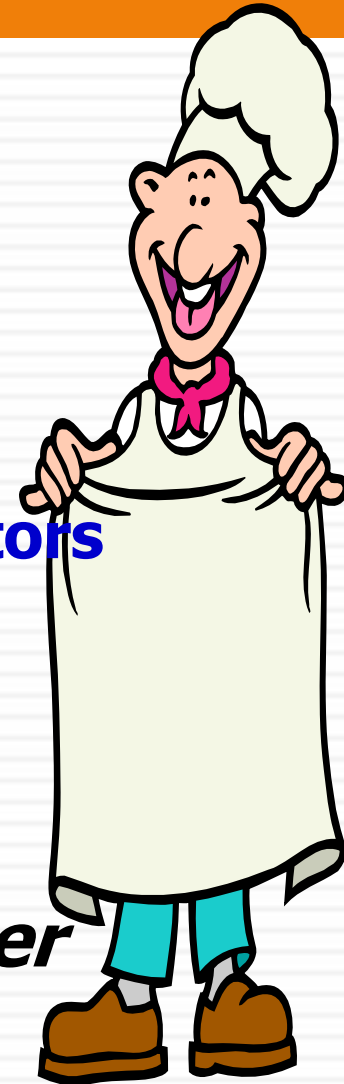


# Energy Losses

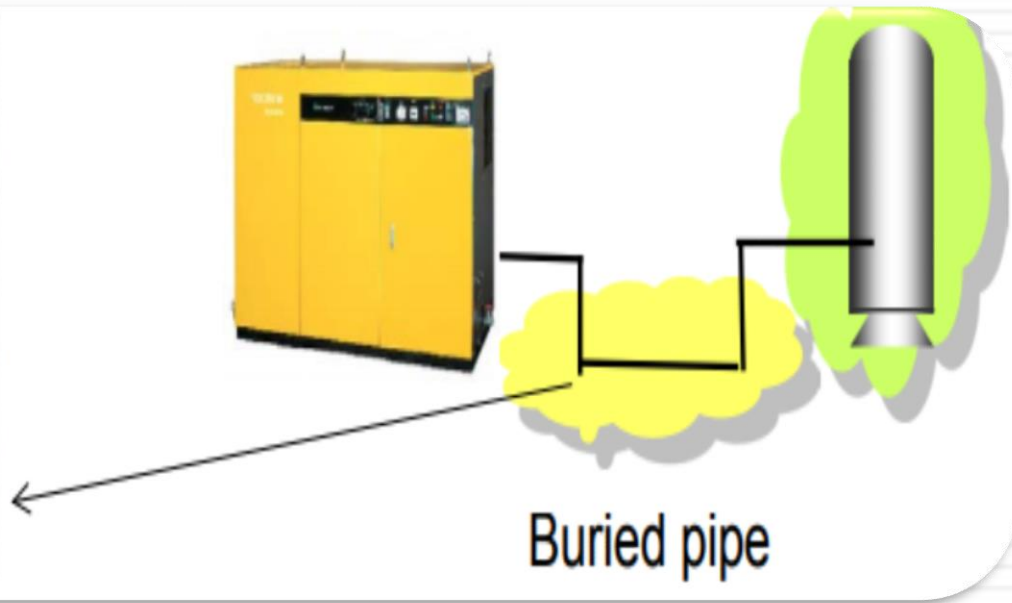
***System Losses waste 20%!!***

- **Pressure Loss in Pipelines, Bends & Valves**
- **Air Leakages from Corroded Pipe**
- **Pressure Loss in After Coolers, Moisture Separators**
- **Air leakages in joints & end connections**
- **Pressure Loss across Filters & Dryers**

***Leading to Compressor operation at Higher Pressure to overcome these losses!***



# Inefficient Piping Layout



# Minimise Leakages

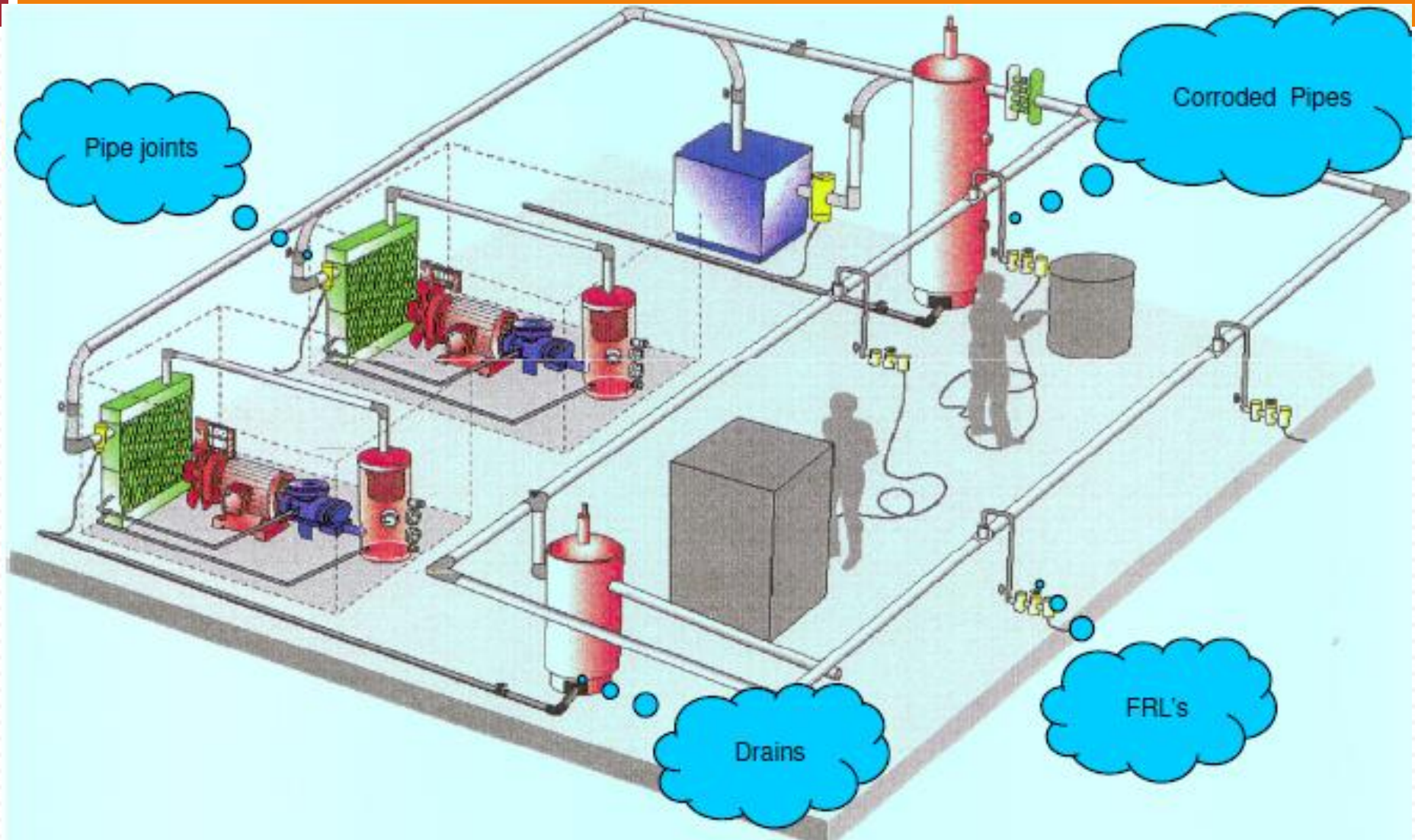
- Common in all industries
- Tricky
- Quantification



**God has given abundant air, which is free!!**

**But ... compressed air is not free!!**

# Common Leak Locations



# Common Leak Locations



Valves



Air Gun



Regulator



Hose Joint



Coupler



Hoses

# Leakage Test

- Close all user points
- Charge the lines
- **Note:** On-load time of compressor (T)  
Off-load time of compressor (t)
- Q : Capacity of compressor

$$\text{Air leakage : L} = \left( \frac{T}{T + t} \right) \cdot Q$$

$$\% \text{ air leakage} = \frac{\text{Air leakage}}{\text{Compressor capacity}} \times 100$$

# Cost Of Leakage At 7kg/cm<sup>2</sup>

Orifice (mm)	Air Leakage (CFM)	Power Wasted (kW)	Annual Savings @ Rs 5/kWh
1.6	6.5	1.26	Rs 0.60 Lakhs
3.2	26	5.04	Rs 2.40 Lakhs
6.4	104	20.19	Rs 7.25 Lakhs



# Optimal Utilisation of Compressors

37 kW Compressor  
Loading – 30 % (27 kW)  
Unloading – 70 % (9 kW)



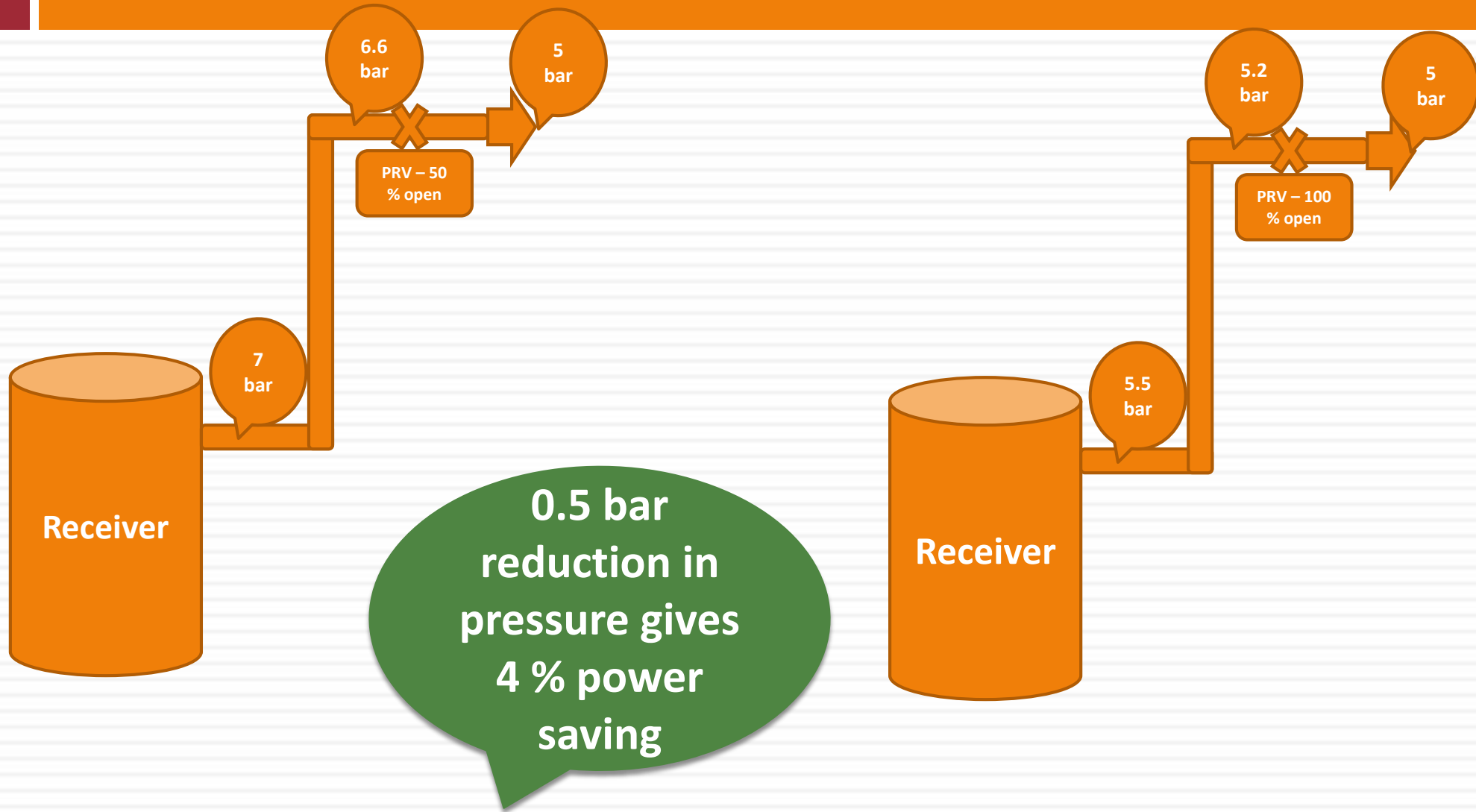
Install new 15 kW  
Compressor  
Use existing compressor as  
standby



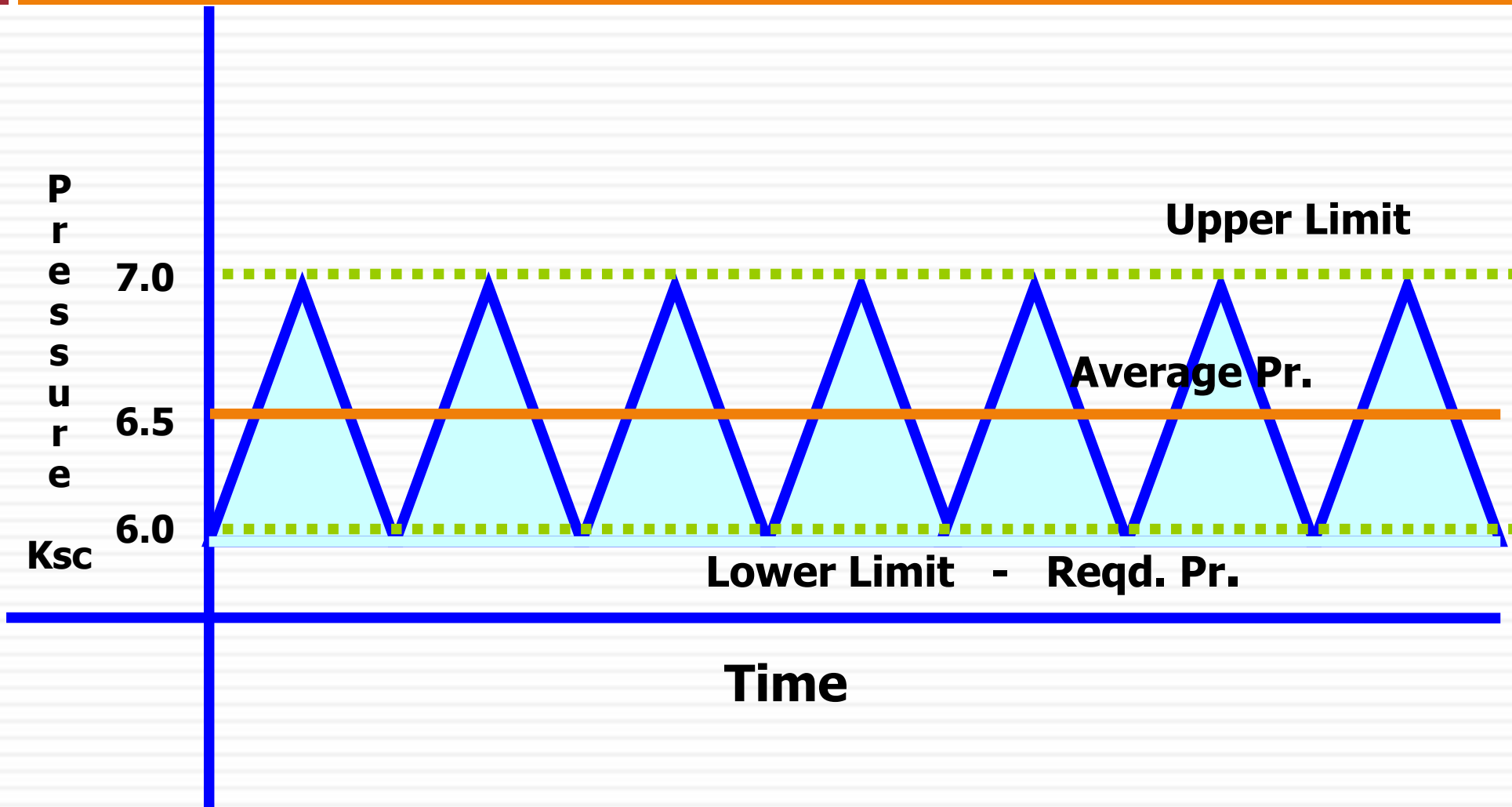
Rs 0.5 Lakhs Savings  
<12 Months Payback



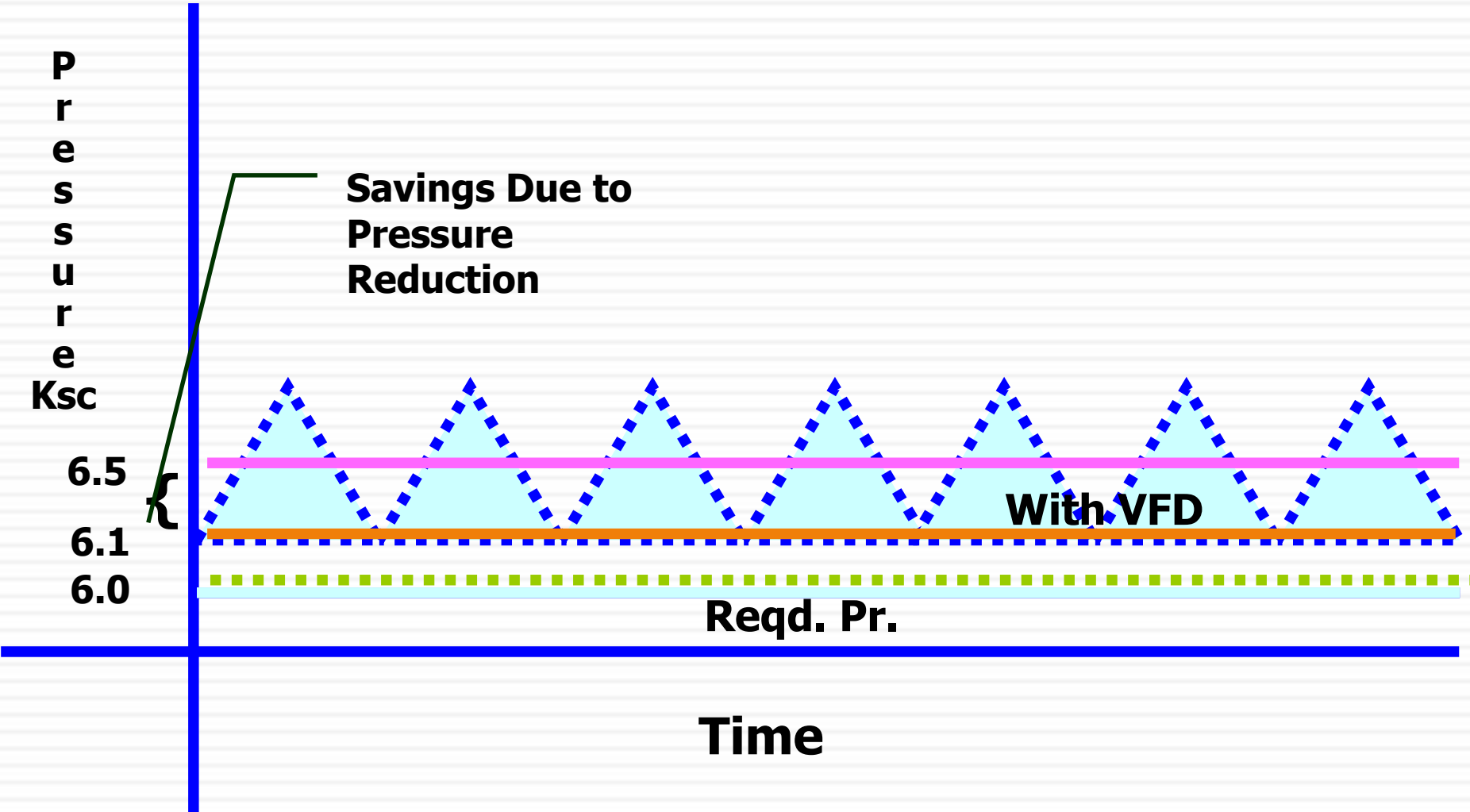
# Pressure Reduction



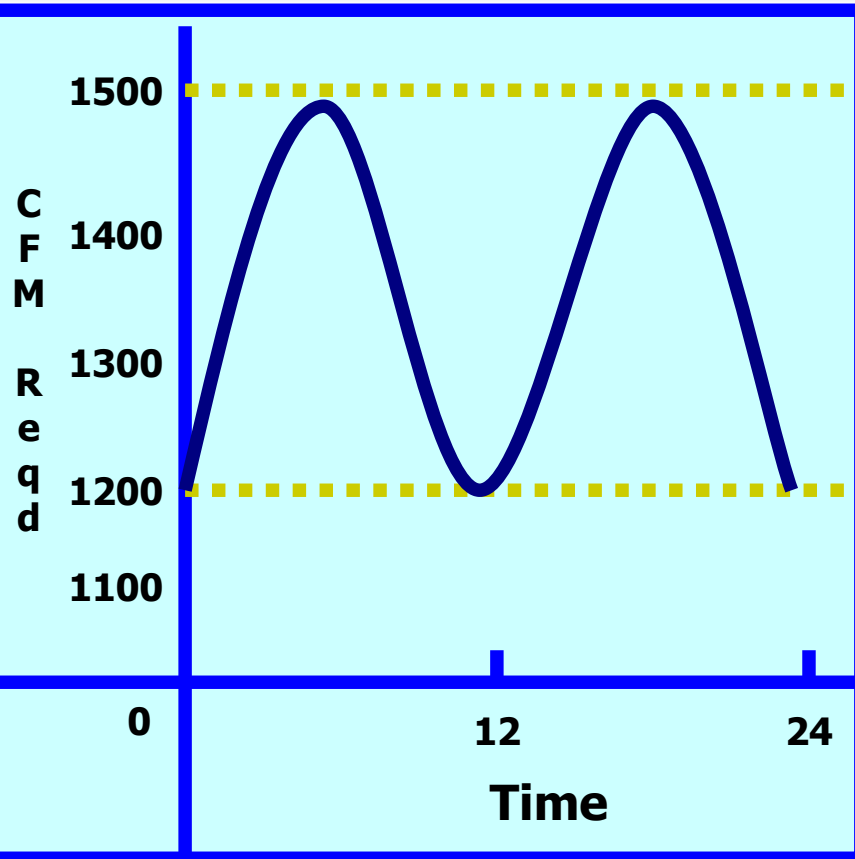
# Concept - Conventional Control



# Concept - VFD Control

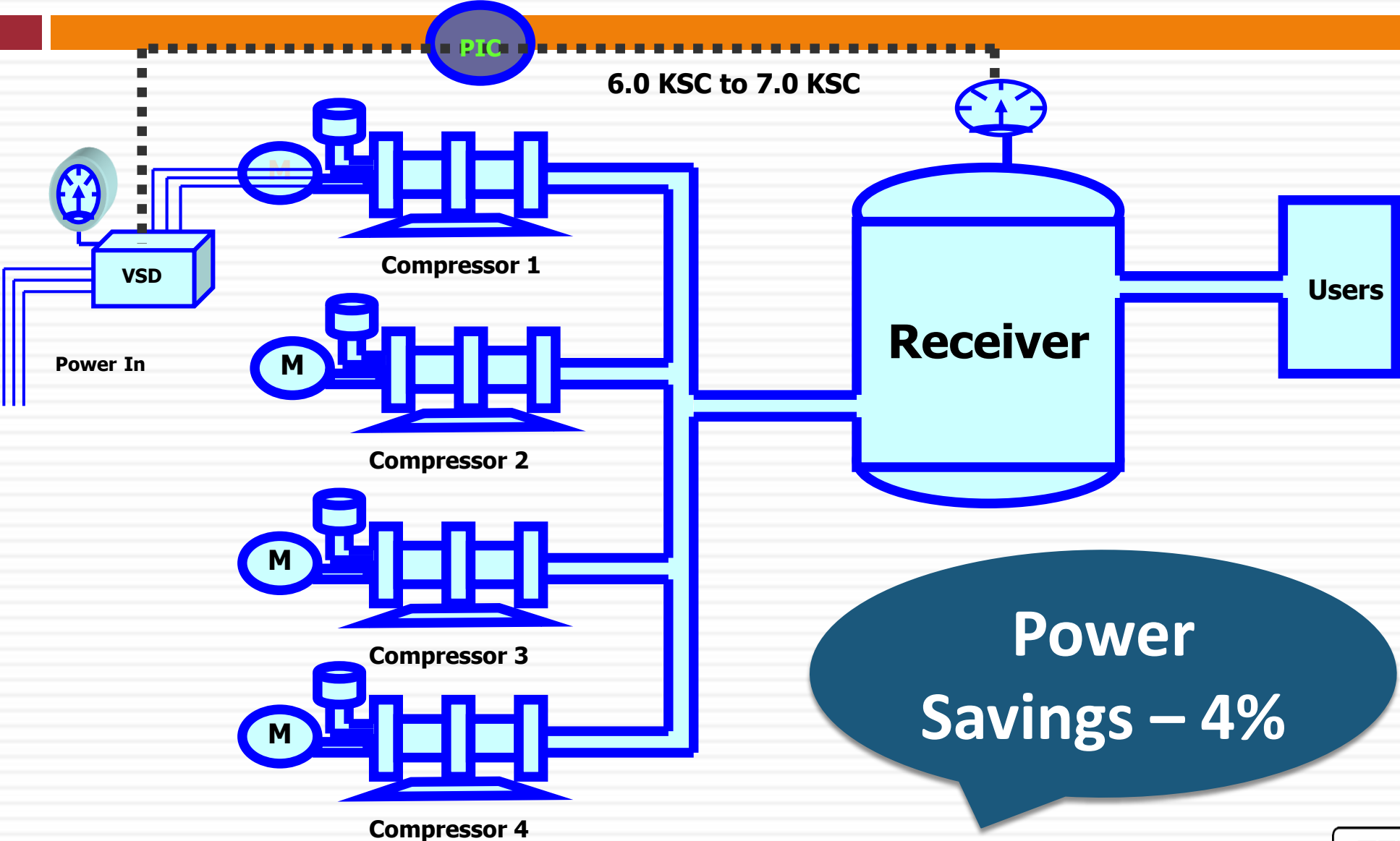


# Savings in Unload Power

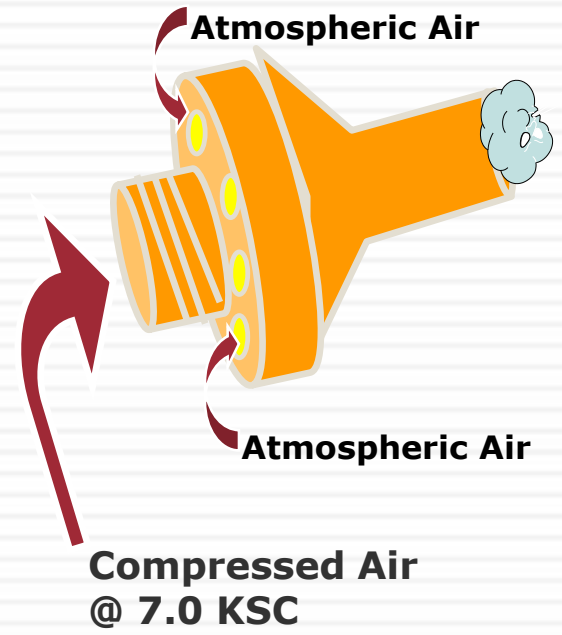
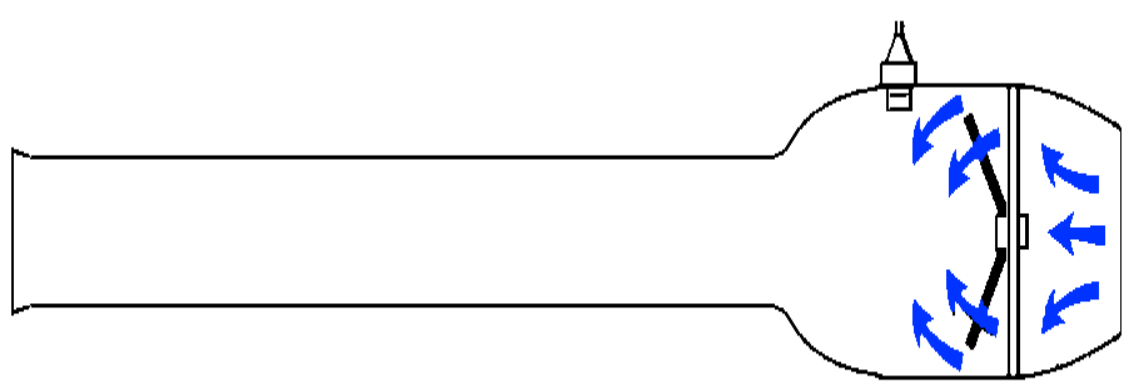


- ❖ **Compressors Designed to meet Fluctuating Load**
- ❖ **Fluctuating Load Leads to Load / Unload**
- ❖ **Lean Time - Unload**
- ❖ **Unload power 15 - 40%**
- ❖ **No useful work**
- ❖ **VSD Avoids Unloading of Compressors**

# Install VFD for One Compressor



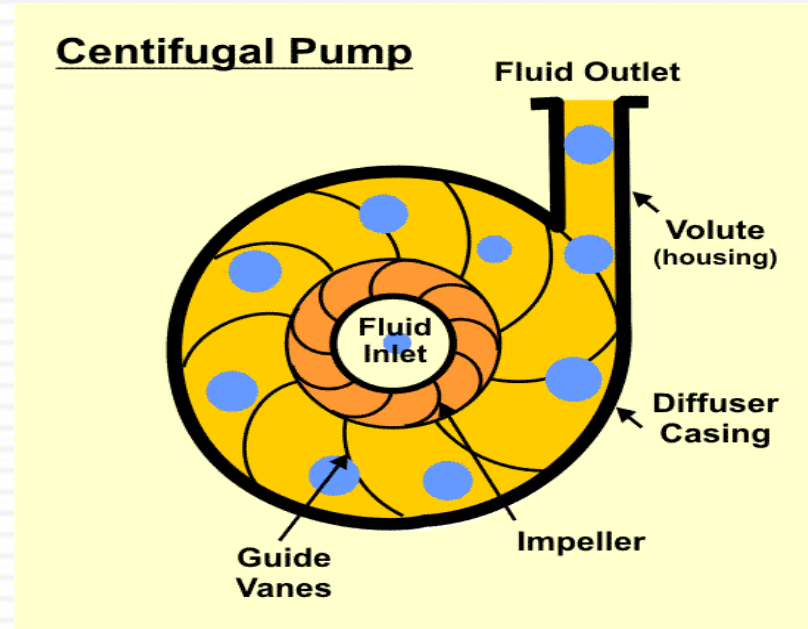
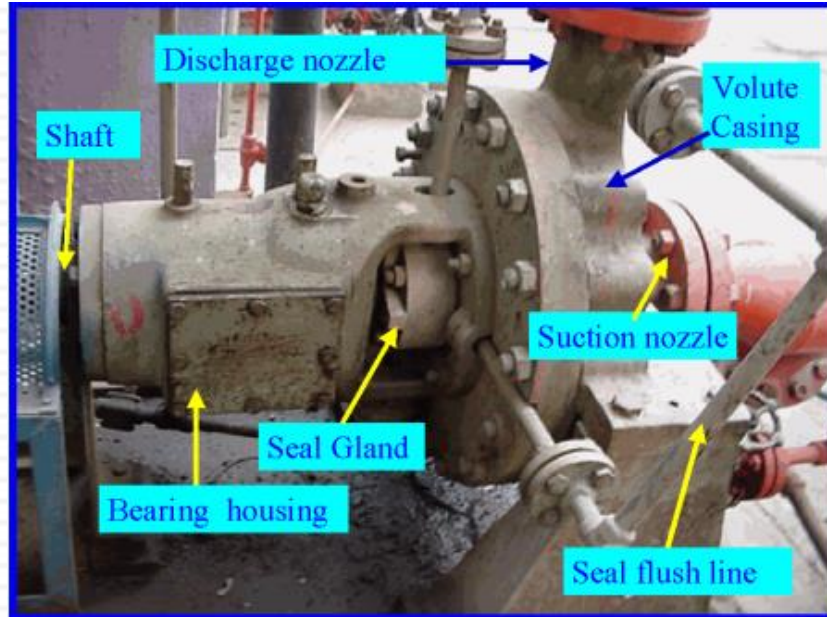
# Use Transvector Nozzle In Air Hose



# PUMPING SYSTEM



# Centrifugal Pumps

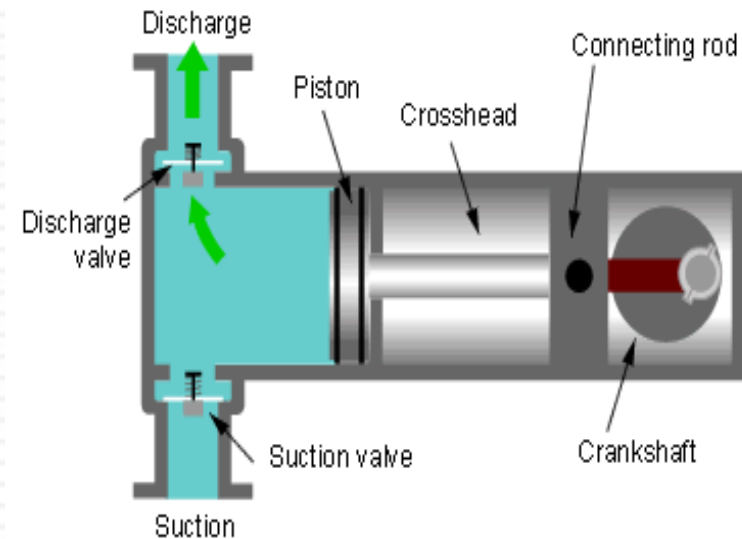
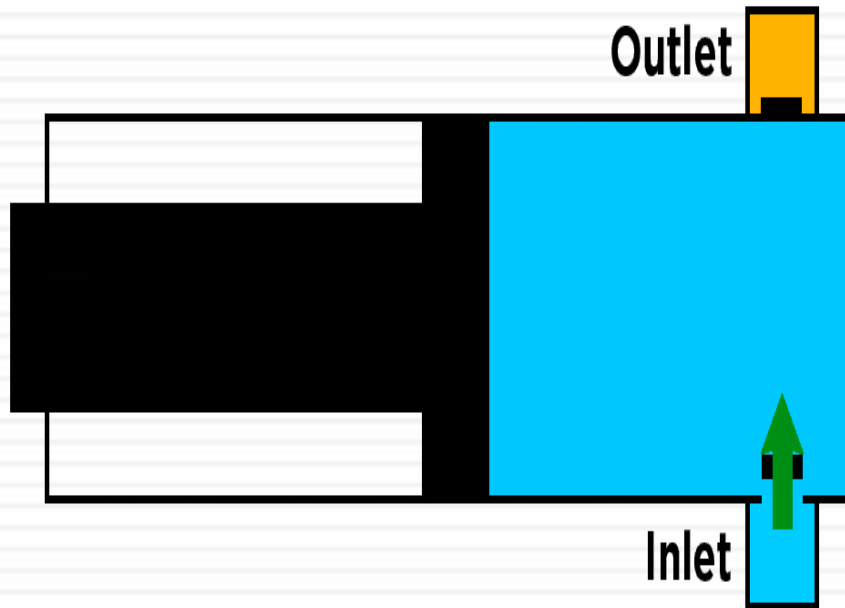


## Centrifugal

- ❖ Moderate pressure (upto 6000 m WC)
- ❖ Moderate capacity (upto 10,000 m<sup>3</sup>/h)
- ❖ General applications



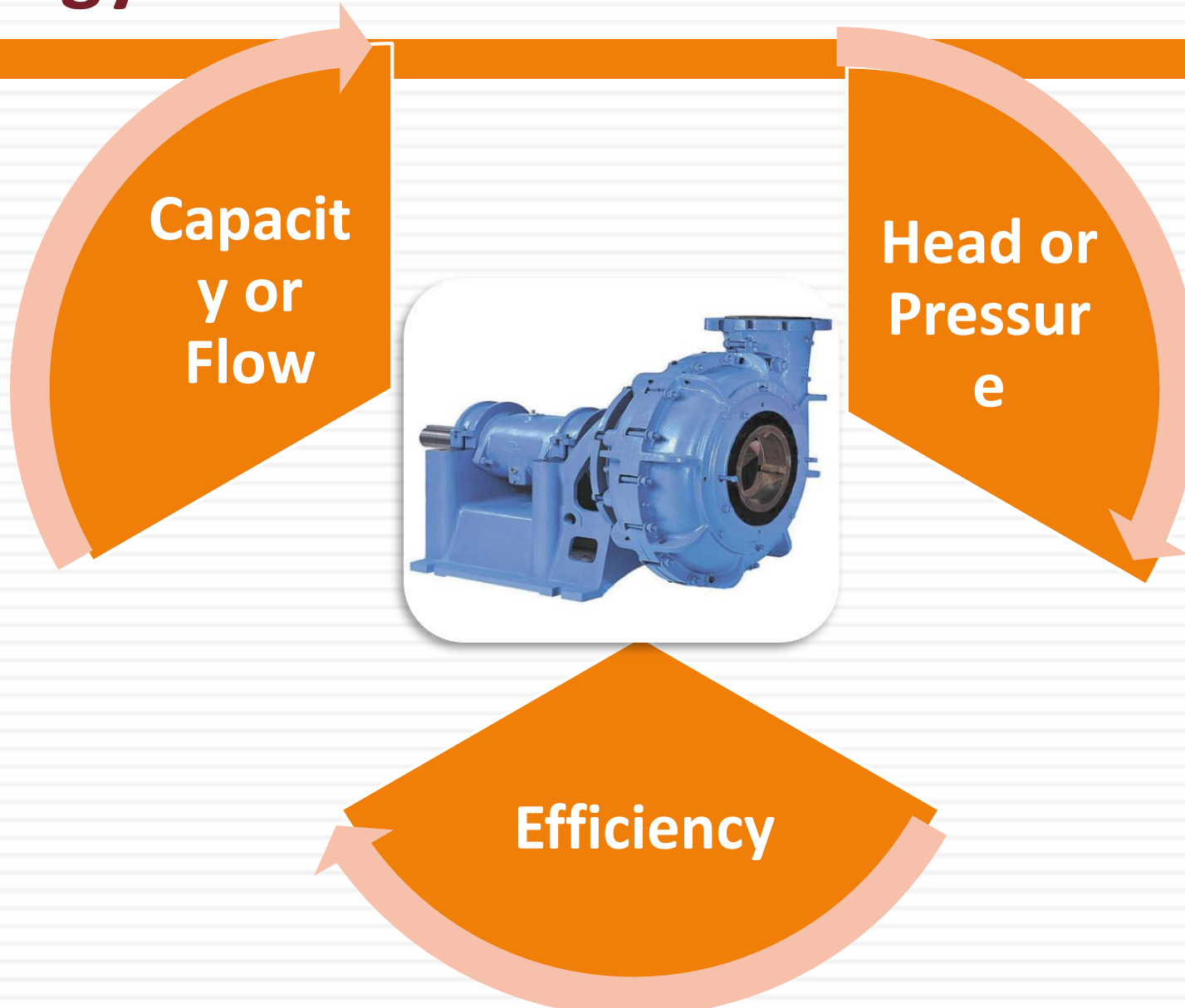
# Positive Displacement Pumps



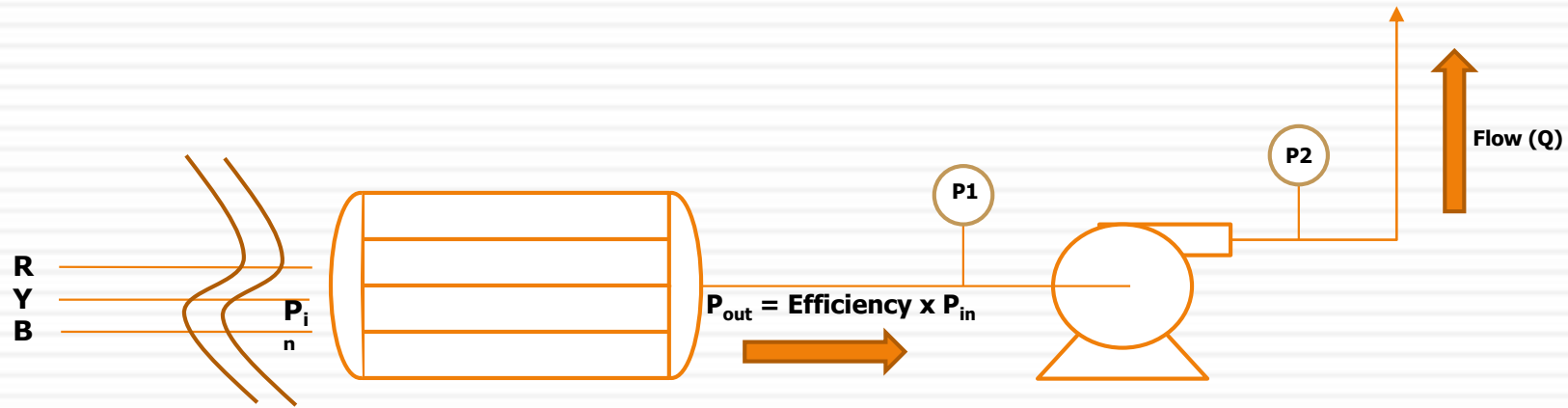
## Reciprocating

- ❖ High pressure - upto 10,000 m WC
- ❖ Low capacity - upto 1000 m<sup>3</sup>/h
- ❖ Lubrication oil pumps

# Energy Parameters



# Efficiency of Pump



$$\text{Pump } \eta (\%) = \frac{\text{Flow (lps)} \times (h_2 - h_1) \text{ (m)} \times \text{Sp. Gr.}}{102 \times P_{out}}$$

# Pumps Formulae

❖ **Capacity**  $\propto$  **(RPM)**

❖ **Head**  $\propto$  **(RPM)<sup>2</sup>**

❖ **Power**  $\propto$  **(Capacity x Head)**

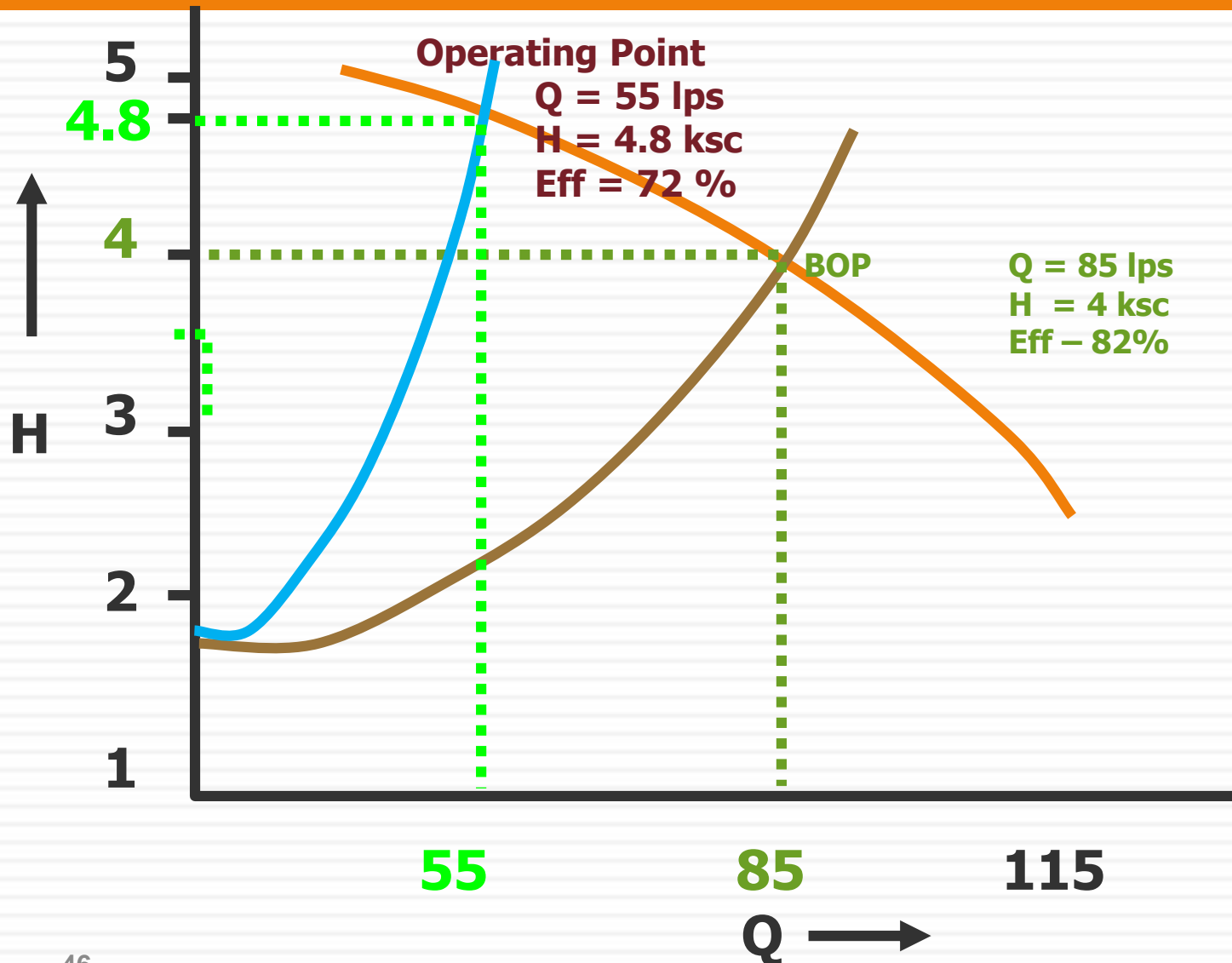
$\propto$  **(RPM)<sup>3</sup>**

# Pumps Formulae

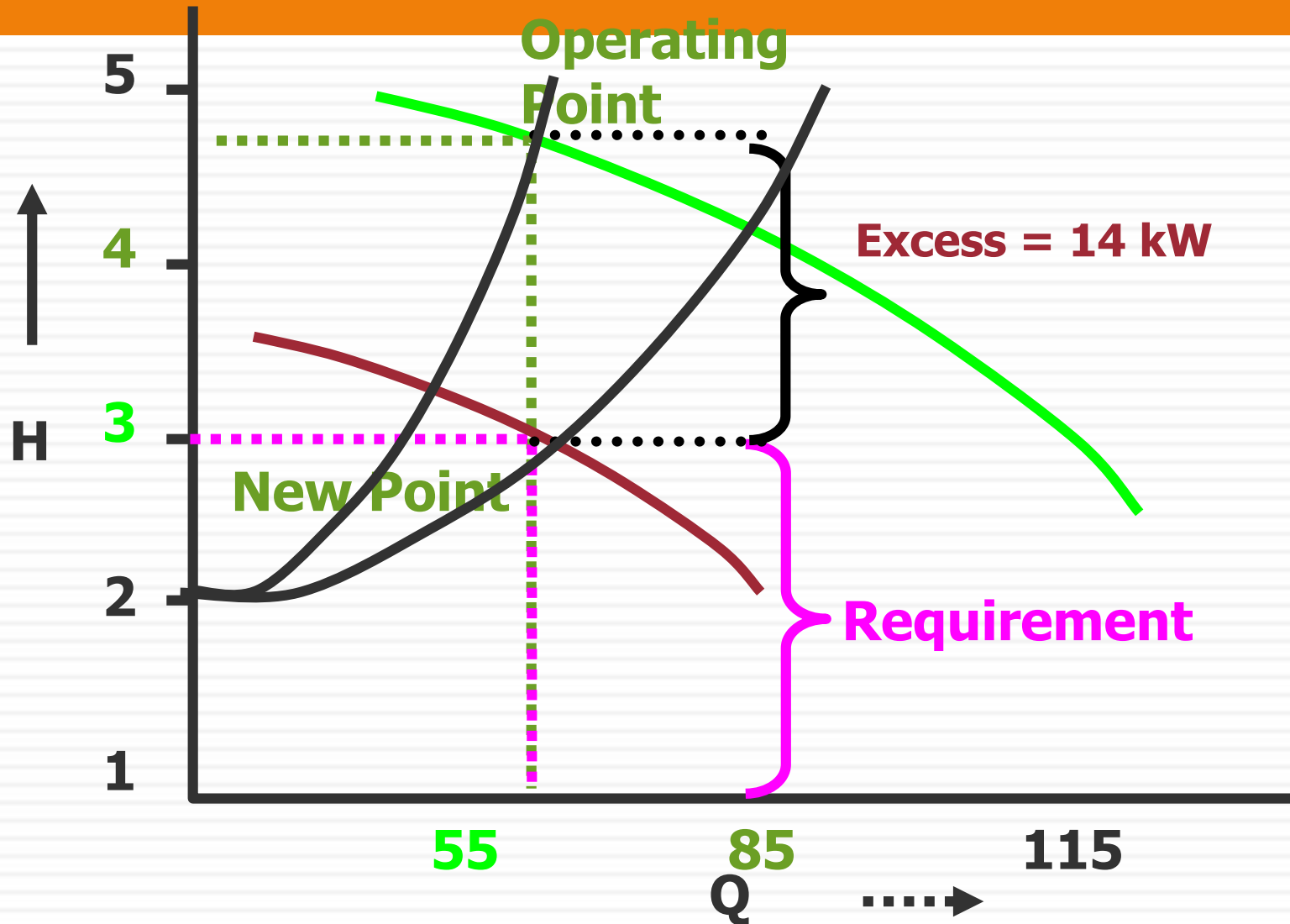
**If the RPM is reduced by say 10%, what will happen to the**

- ❖ **Capacity** : **reduces by 10%**
- ❖ **Head** : **reduces by 19%**
- ❖ **Power** : **reduces by 27%**

# Operating Conditions of Pump

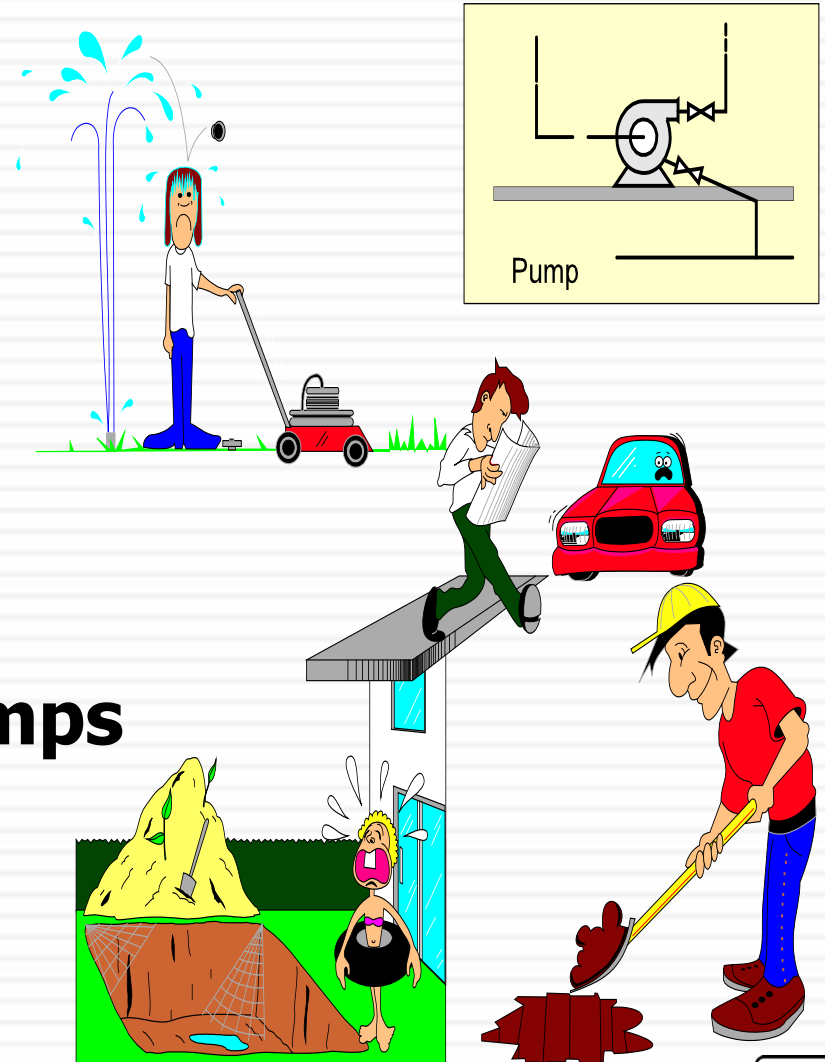


# Operating Conditions of Pump



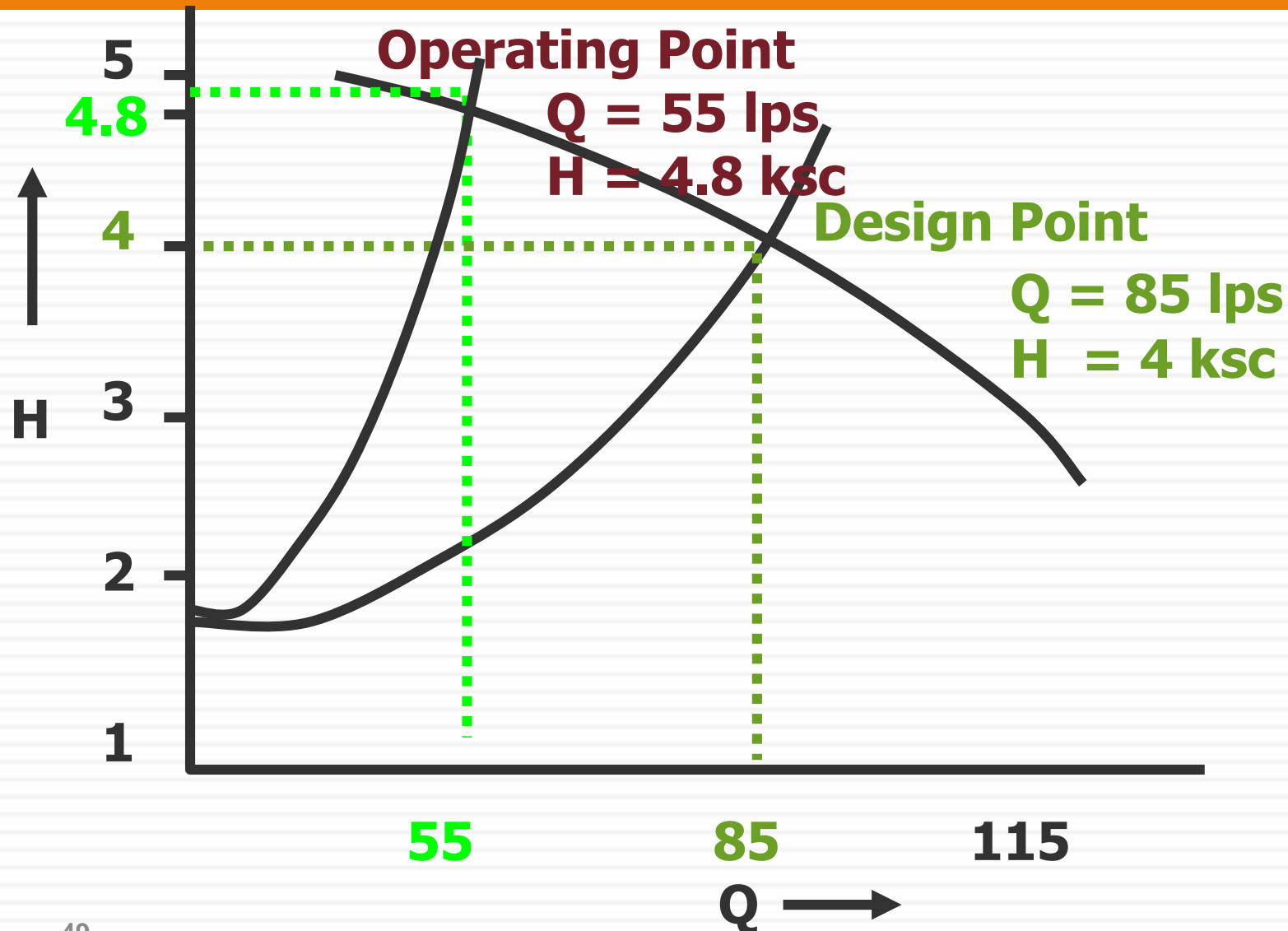
# Reasons for excess power consumption

- ❖ **Wrong Selection**
- ❖ **Over Design**
- ❖ **Improper Layout**
- ❖ **Old inefficient pumps**
- ❖ **Multiple smaller size pumps**

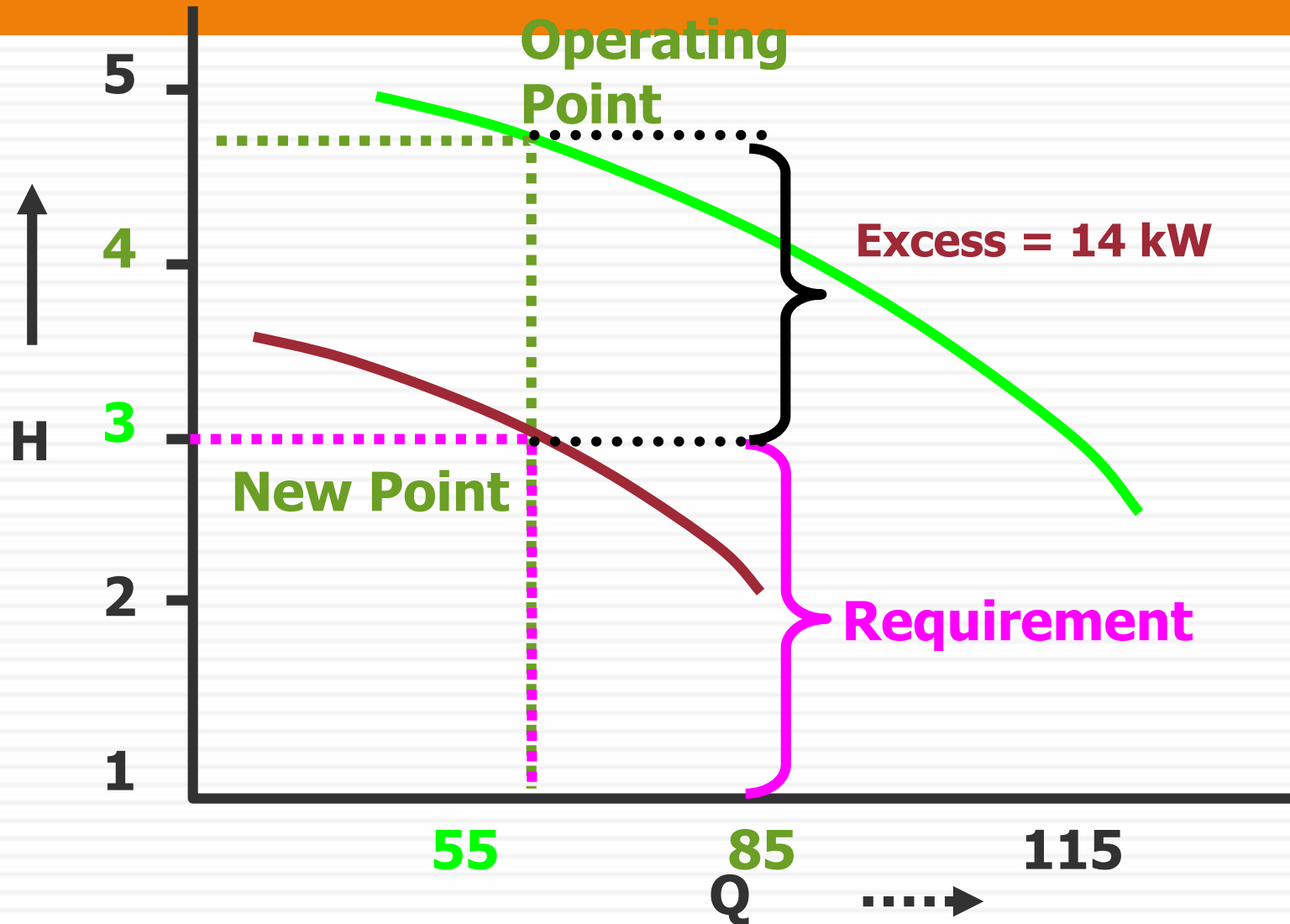




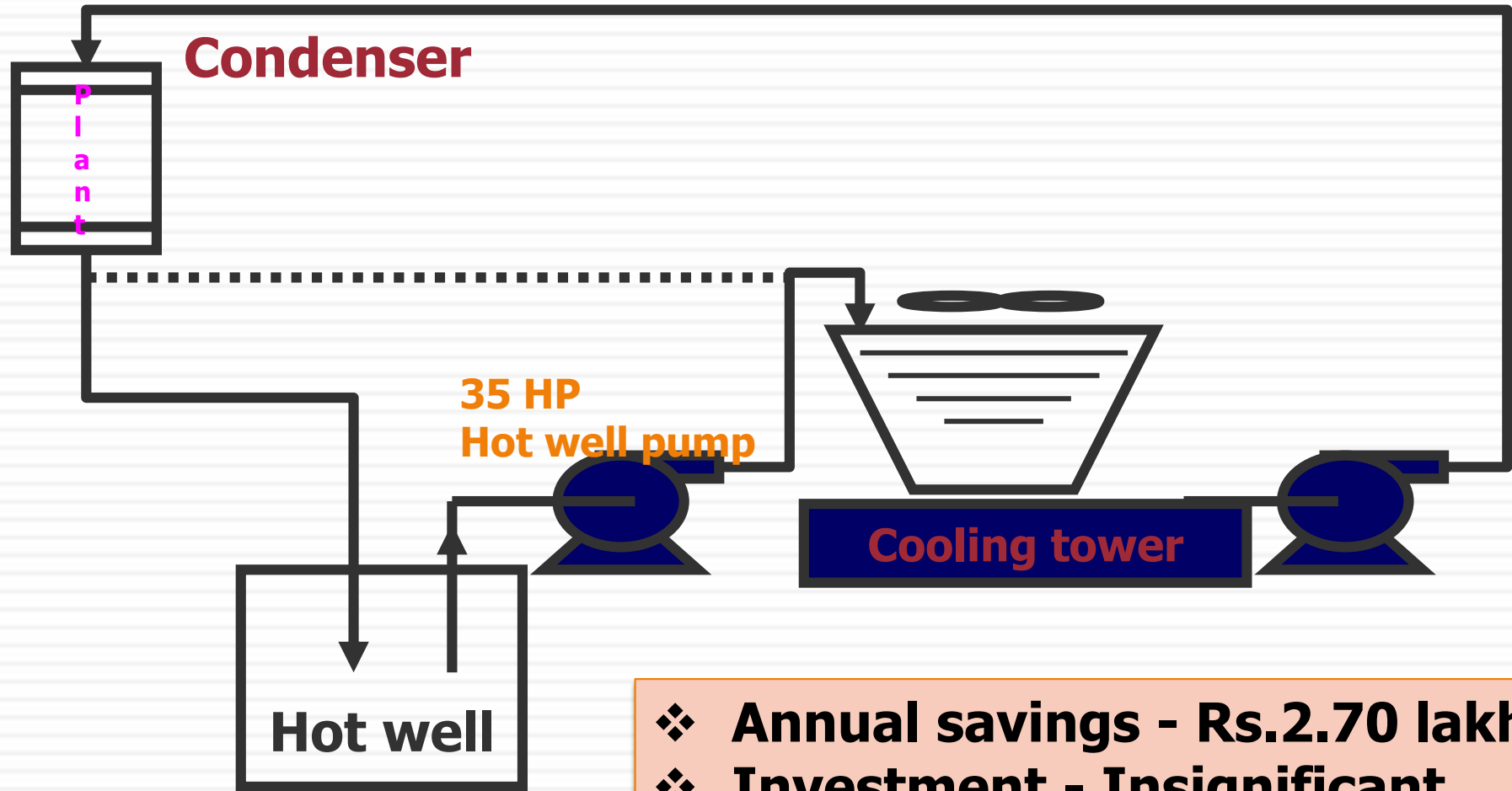
# Operating Conditions of Pump



# Operating Conditions of Pump



# Use Gravity Flow as Much as Possible



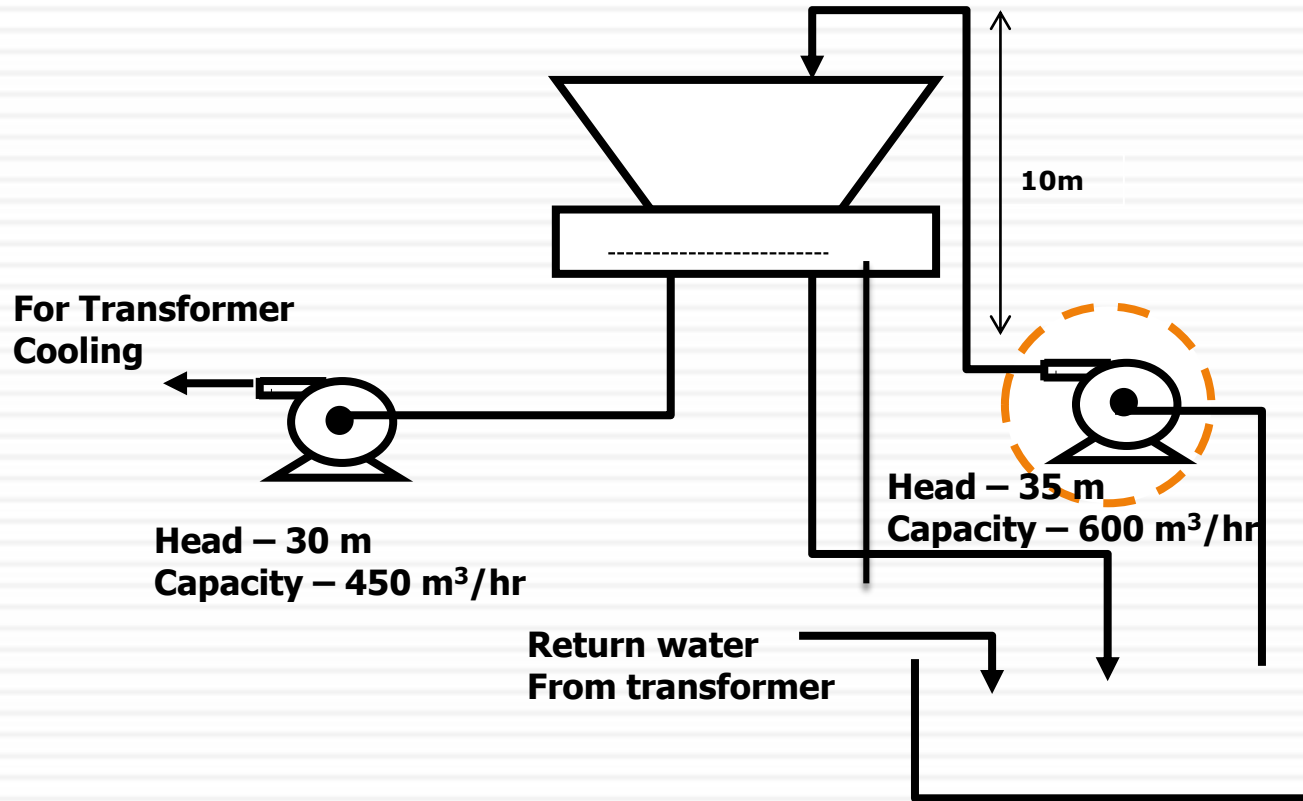
- ❖ Annual savings - Rs.2.70 lakhs
- ❖ Investment - Insignificant

# Methodology of Pump Survey

- ❖ **Is the pump correctly Sized ?**
  - **Excess capacity due to uncertainty**
- ❖ **Leads to operation with valve throttling**
  - **Energy inefficient practice**

- ❖ **Impeller reduction**
- ❖ **Low capacity/head pump**
- ❖ **Installation of variable speed drive**

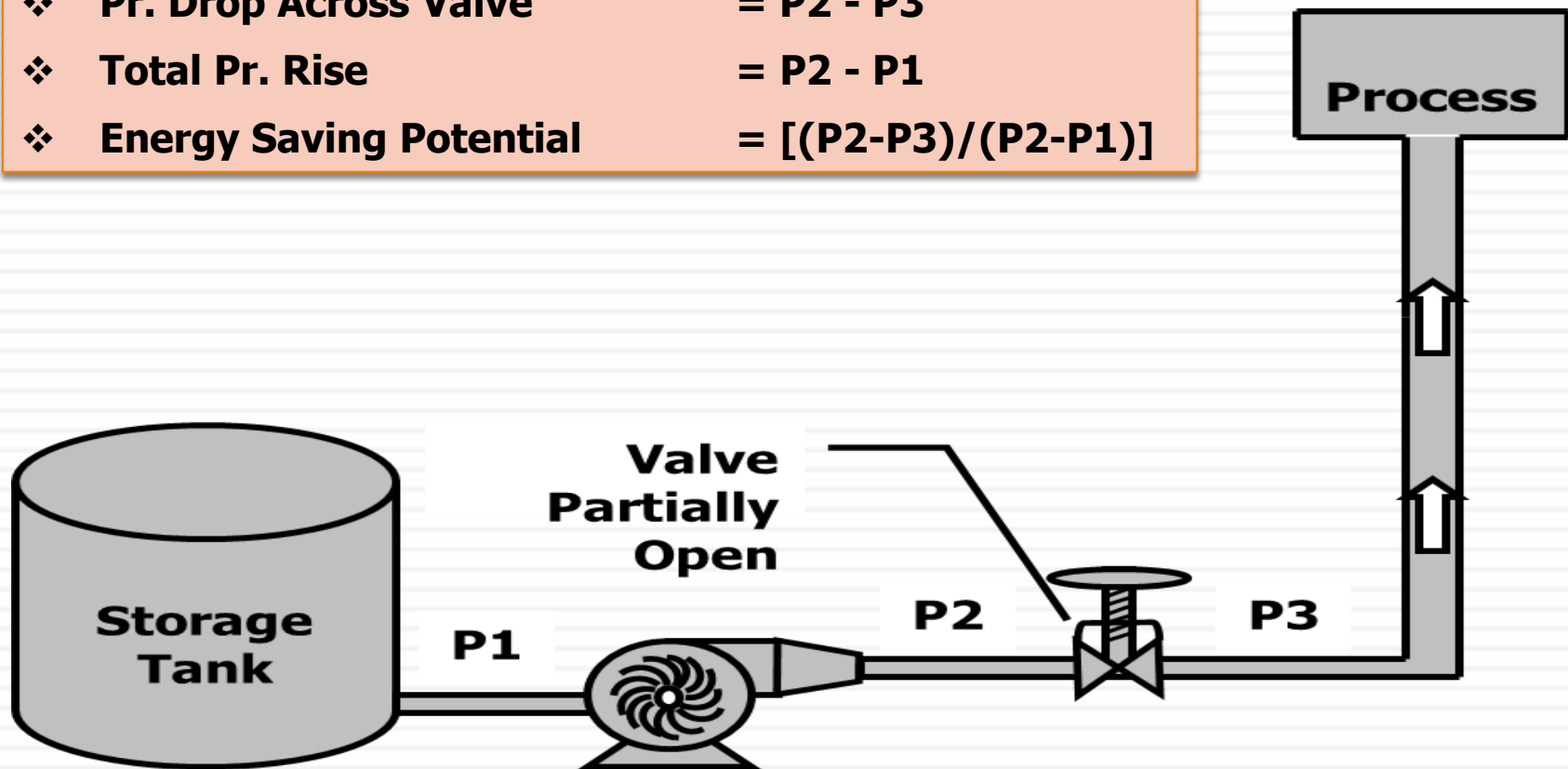
# Installation of correct size pump



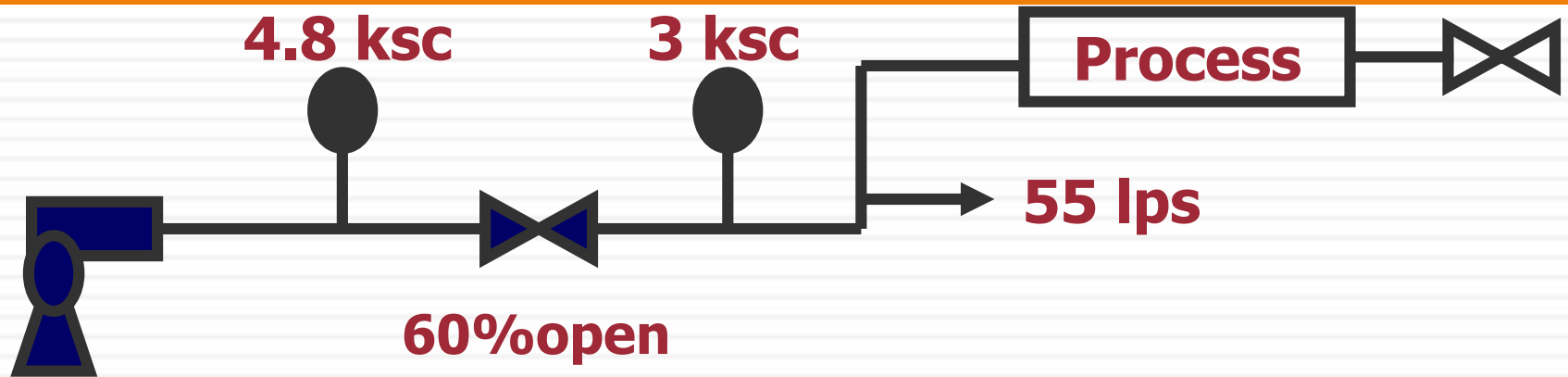
<b>Annual savings</b>	-	<b>Rs 7.29 Lakhs</b>
<b>Investment</b>	-	<b>Rs 3.00 Lakhs</b>
<b>Payback period</b>	-	<b>5 months</b>

# Pressure Drop Across Valve

- ❖ Pr. Drop Across Valve =  $P2 - P3$
- ❖ Total Pr. Rise =  $P2 - P1$
- ❖ Energy Saving Potential =  $[(P2 - P3) / (P2 - P1)]$



# Effect of Valve Throttling



## Design

**Capacity = 85 lps**

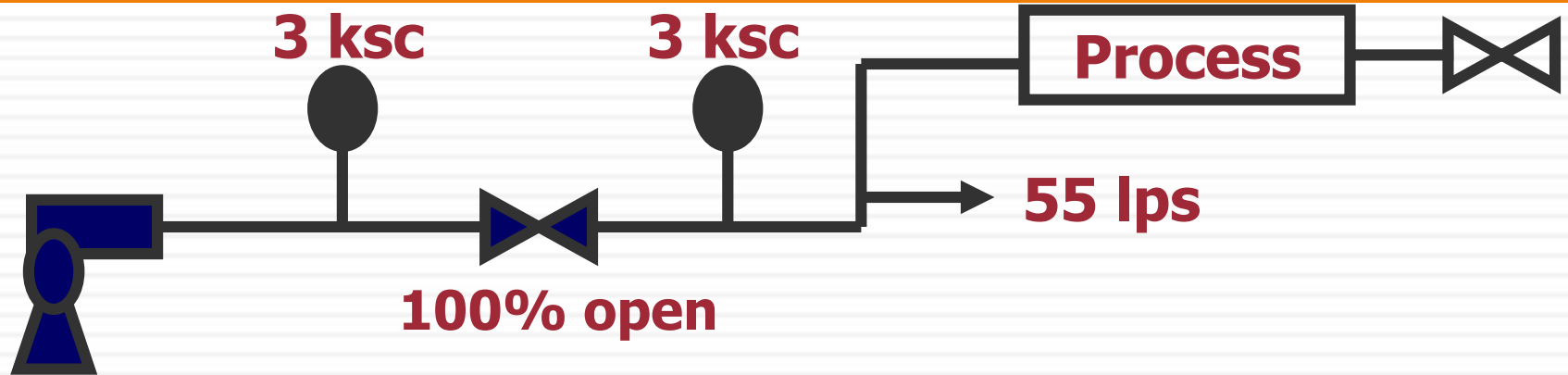
**Head = 4 ksc**

**Existing = 4.8 ksc**

**$kW_{EX} = 55 \times 48 / (102 \times 0.7)$**

**= 37.0 kW**

# Effect of Valve Throttling



## Modified

**Proposed = 3.0 ksc**

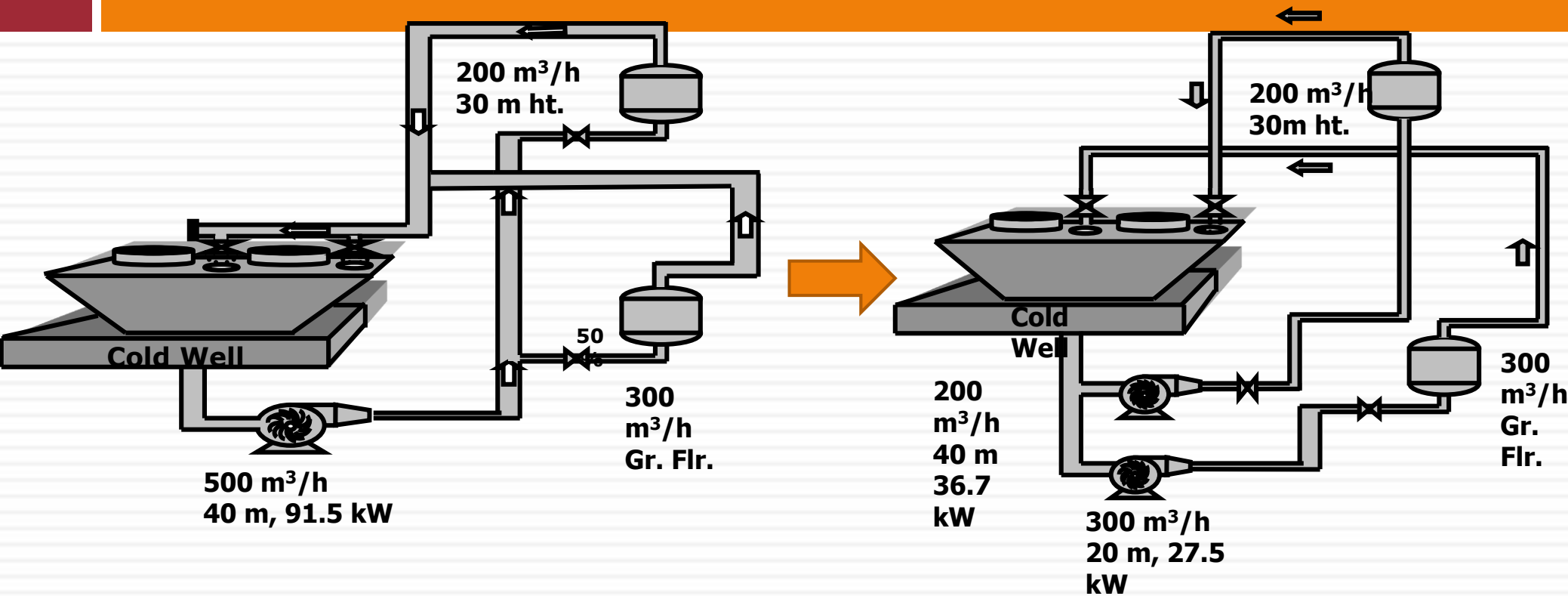
**kW<sub>p</sub> = 55 x 30 / (102 x 0.7)**

**= 23.0 kW**

**Savings = 14 kW**

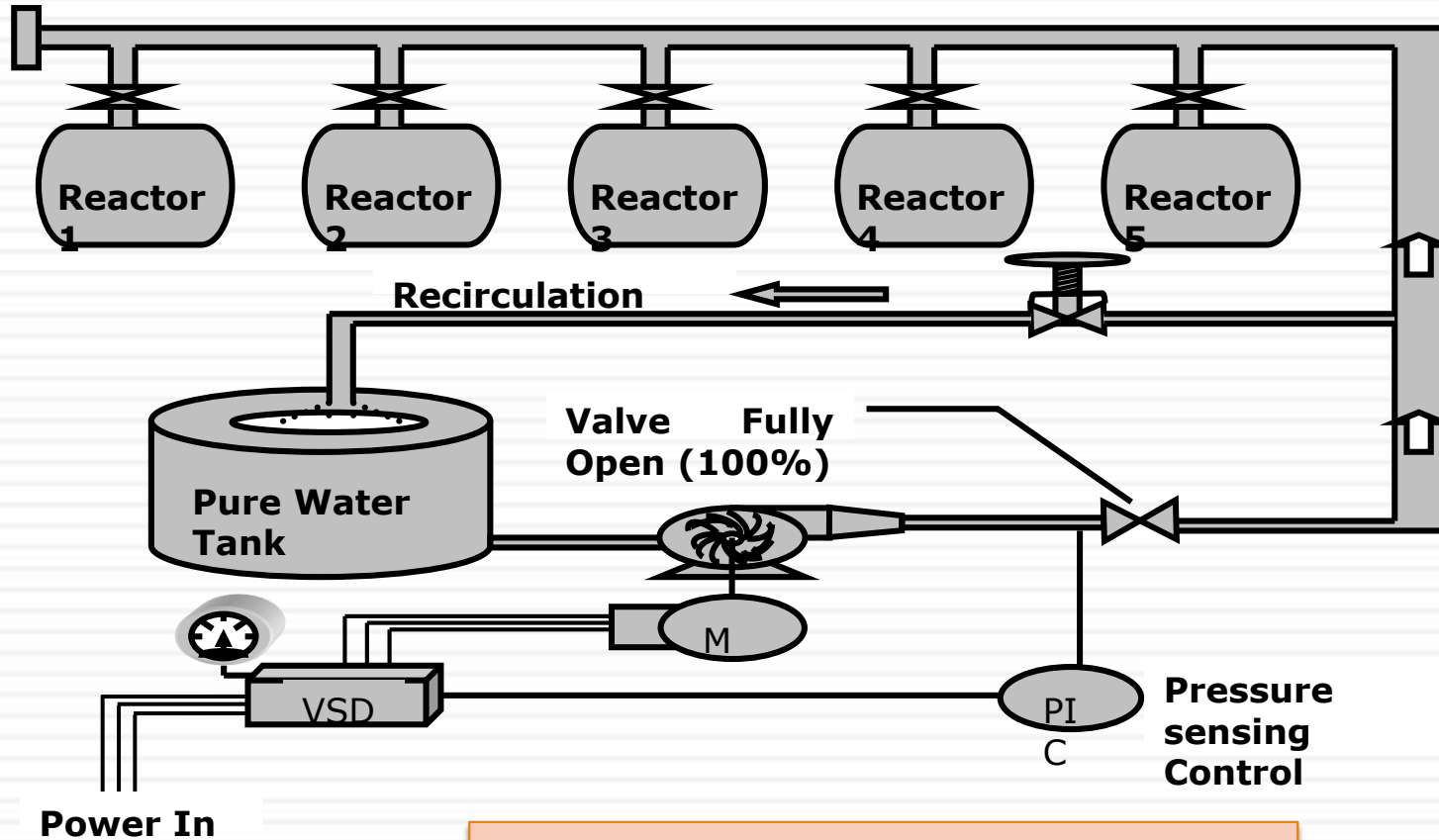


# Segregate high and low head users



<b>Annual Savings</b>	<b>= Rs. 4.80 Lakhs</b>
<b>Investment</b>	<b>= Rs. 6.00 Lakhs</b>
<b>Payback period</b>	<b>= 15 Months</b>

# VFD for Pumping system



Annual savings	- Rs.3.00 Lakhs
Investment	- Rs.2.00 Lakhs
Payback period	- 8 Months

# Install TIC for the cooling tower fan

## ❖ Present system

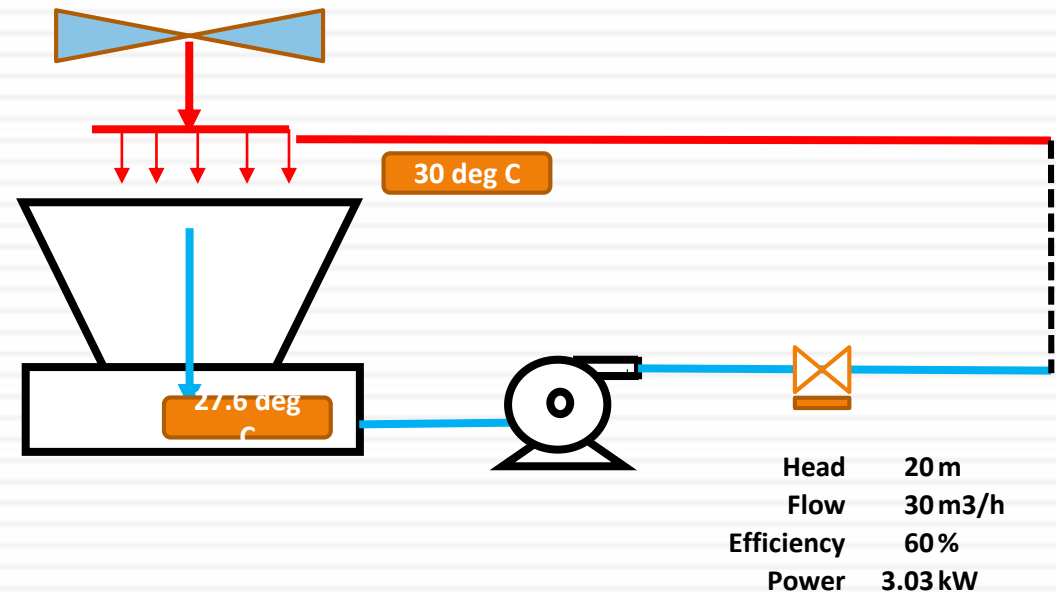
### ▣ Two Pumps

- One running and one standby

### ▣ Cooling tower fan running continuously,

- No control on the CT fan speed

### ▣ $DT = 2.4 \text{ degC}$



# Install TIC for the cooling tower fan

## ❖ Recommendation

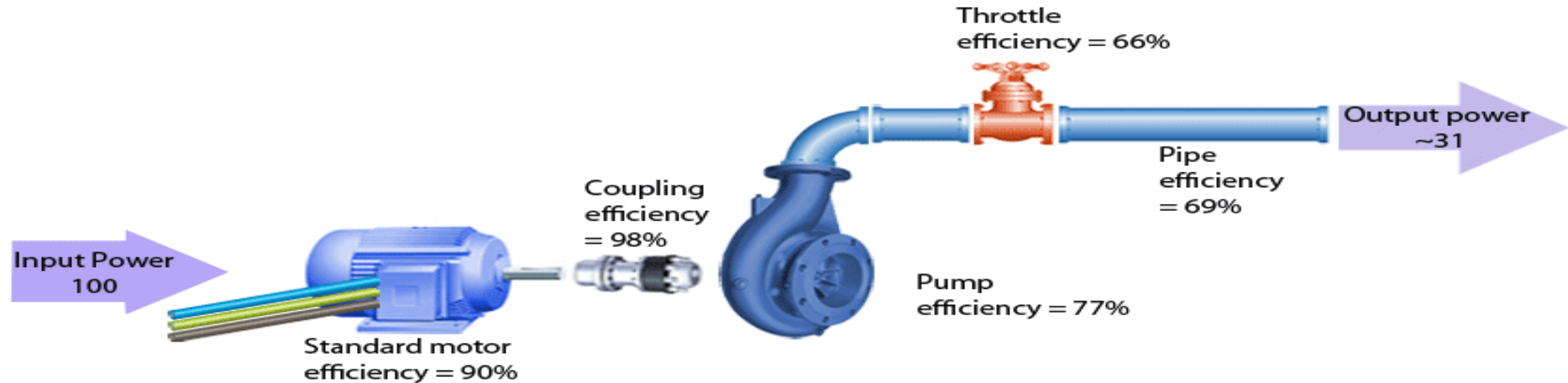
- ❑ Install TIC and control fan operation
- ❑ Automate CT fan operation based on the cold well temperature
  - CT fan switch OFF if cold well water temperature lesser than 24 °C
  - CT fan switch ON if cold well water temperature greater than 27 °C
- ❑ Savings can be achieved during favorable conditions

# Install TIC for the cooling tower fan

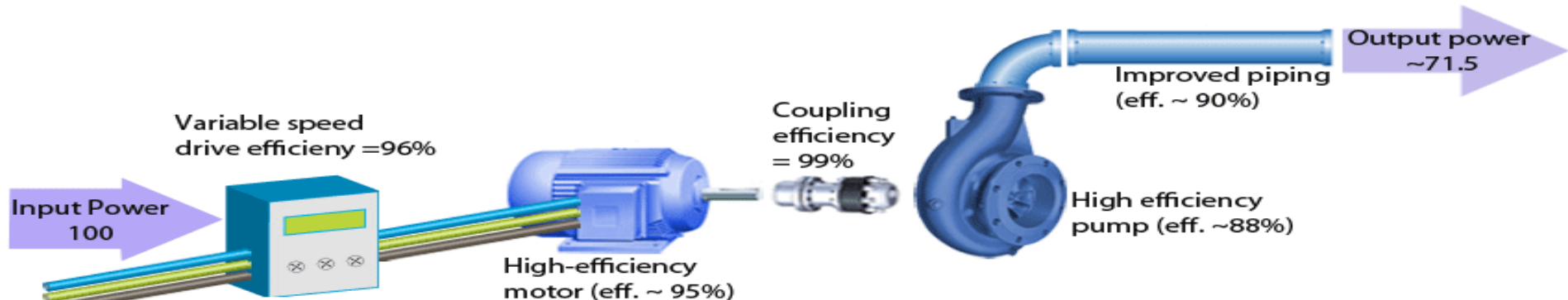
<b>Annual Saving</b>	-	<b>Rs 3700</b>
<b>Investment</b>	-	<b>Rs 2000</b>
<b>Payback</b>	-	<b>6 months</b>

# Energy Efficient Pumping System

## Conventional Pumping System (Efficiency ~ 31%)



## Efficiency Optimized Pumping System (Efficiency ~ 72%)



**Thank You....**